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(54) Title: SCREW EXTRUDER WITH IMPROVED DISPERSIVE MIXING ELEMENTS <div data-bbox="386 1136 1224 1610"> </div> (57) Abstract <p>A screw extruder (10) having a barrel (18) which has a bore (26) defining an inner surface (44) and one or more extruder screws (28), positioned within the bore (26). The extruder screw or screws (28) include a central shaft (34) and one or more screw flights (30). The extruder screw or screws (28) further including one or more dispersive mixing elements (204, 234, 308, 406, 508, 558), which interact with the inner surface of the barrel (44) to form one or more progressively narrowing passages (46) through which material is forced into multiple regions of high elongational and shear stress (480, 120, 214, 310, 410, 510, 564). A second preferred embodiment is a screw extruder (10) having a barrel (18) having a bore (26) defining an inner surface (44) and one or more extruder screws (600, 701), positioned within the bore (26). The extruder screw or screws (600, 701) include a central shaft (602, 706) and a number of dispersive mixing elements (604, 608, 714), which are configured and positioned to form a number of progressively narrowing passages (606, 716) through which material is forced into multiple regions of high elongational and shear stress (608, 718).</p>		

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SCREW EXTRUDER WITH IMPROVED DISPERSIVE MIXING ELEMENTS

The following is a continuation-in-part of co-pending application U.S. application 08/966,272 which was filed on 11/07/97.

TECHNICAL FIELD

5 The present invention relates generally to machines for extrusion of materials and more particularly to screw extruders adapted for use with plastics and plastic-like materials. The inventor anticipates that primary application of the present invention will be for the manufacture of color concentrates, polymer blends, and polymer alloys.

BACKGROUND ART

10 A screw extruder is a machine in which material, usually some form of plastic, is forced under pressure to flow through a contoured orifice in order to shape the material. Screw extruders are generally composed of a housing, which is usually a cylindrical barrel section, surrounding a central motor-driven screw. At a first end of the barrel is a feed housing containing a feed opening through which new material, usually plastic particles, is
15 introduced into the barrel. The screw contains raised portions called flights having a larger radial diameter than the screw's central shaft and which are usually wrapped in a helical manner about the central shaft. The material is then conveyed by these screw flights toward the second end of the barrel through a melting zone, where the material is heated under carefully controlled conditions to melt the material, and then passes through a melt-
20 conveying zone, also called a pumping zone. The melted plastic is finally pressed through a shaped opening or die to form the extrudate.

Besides conveying material toward the die for extrusion, the screw is depended upon to perform mixing of the feed material. Very generally, mixing can be defined as a process to reduce the non-uniformity of a composition. The basic mechanism involved is to induce
25 relative physical motion in the ingredients. The two types of mixing that are important in screw extruder operation are distribution and dispersion. Distributive mixing is used for the purpose of increasing the randomness of the spatial distribution of the particles without reducing the size of these particles. Dispersive mixing refers to processes that reduce the size of cohesive particles as well as randomizing their positions. In dispersive mixing, solid
30 components, such as agglomerates, or high viscosity droplets are exposed to sufficiently high stresses to cause them to exceed their yield stress, and they are thus broken down into smaller particles. The size and shape of the agglomerates and the nature of the bonds holding the

agglomerate together will determine the amount of stress required to break up the agglomerates. The applied stress can either be shear stress or elongational stress and generally, elongational stress is more efficient in achieving dispersion than is shear stress.

An example of dispersive mixing is the manufacture of a color concentrate where the
5 breakdown of pigment agglomerates below a certain critical size is crucial. An example of distributive mixing is the manufacture of miscible polymer blends, where the viscosities of the components are reasonably close together. Thus, in dispersive mixing, there will always be distributive mixing, but distributive mixing will not always produce dispersive mixing.

10 In extrusion processes, the need for good dispersive mixing is often more important than for distributive mixing. This is particularly true in the extrusion of compounds which contain pigments which must be uniformly mixed or small gage extrusion such as spinning of fibers or extrusion of thin films.

In screw extruders, significant mixing occurs only after the polymer has melted. Thus, the mixing zone is thought of as extending from the start of the melting zone to the end
15 of the extrusion die. Within this area there will be considerable non-uniformities in the intensity of the mixing action and the duration of the mixing action, both in the barrel section and in the extrusion die. In molten polymer, the stress is determined by the product of the polymer melt viscosity and rate of deformation. Therefore, in general, dispersive mixing should be done at as low a temperature as possible to increase the viscosity of the fluid, and
20 with it, the stresses in the polymer melt.

Fluid elements are spoken of as having a "mixing history", which refers to the amount of elongational and shear stress to which it has been exposed, and the duration of that exposure. A polymer element that melts early in the mixing zone process will have a more significant mixing history than one that melts near the end of the melting zone.

25 Generally, in an extruder with a simple conveying screw the level of stress or the fraction of the fluid exposed to it is not high enough to achieve good dispersive mixing. Distributive mixing is easier to achieve than dispersive mixing, but unmodified screws have also been found to produce inadequate distributive mixing for many applications. Therefore, numerous variations in screw design have been attempted in prior inventions to increase the
30 amount of distributive or dispersive mixing in screw extruders. These devices usually contain a standard screw section near the material input hopper, and one or more specially designed sections to enhance mixing. These mixing sections naturally fall into the categories of distributive and dispersive mixing elements.

Varieties of distributive mixing elements are shown in FIG. 2 A – F. Practically any disruption of the velocity profiles in the screw channel will cause distributive mixing. Thus even simple devices, such as the placement of pins (see FIG. 2A) between the screw flights can enhance distributive mixing. FIG 2B shows the well-known Dulmage mixing section, in which the polymer flow is divided into many narrow channels, which are combined and divided again several times. The Saxton mixing section (FIG. 2 C) and the “pineapple” mixing section (FIG. 2D) are used to produce similar results. FIG. 2E shows a screw which has slots cut into the flights. A variation called the Cavity Transfer Mixer is shown in FIG. 2F. There are cavities both in the rotor and the barrel. This type of device reportedly performs both dispersive and distributive mixing.

In addition to these devices, static mixers are often used to divide and recombine the melt stream to intermingle the material and eliminate variations in temperature, composition and mixing history. These generally do not provide regions of high stress, and are thus mostly used for distributive mixing.

The devices shown in FIG. 2 A - F have been primarily classified as distributive mixers because their action is mainly to spatially redistribute material without subjecting it to regions of high shear stress. The variations shown in FIG. 2 G-J are designed to include high shear stress regions and thus perform dispersive mixing.

The most common dispersive mixing section is the fluted or splined mixing section in which one or more barrier flights are placed along the screw so that material has to flow over them. In passing through the barrier clearance, the material is subjected to a high shear rate which acts to break up agglomerates. One such device is the Maddock mixing section, which is shown in FIG. 2 G. The Maddock has longitudinal splines that form a set of semicircular grooves. Alternate grooves are open on the upstream and downstream ends. Material that enters the inlet grooves is forced to pass over the mixing flights, which are shown as cross hatched areas, before reaching the outlet grooves. While passing over the mixing flights, the material is subjected to high shear stress. The disadvantage of this type of mixing element is that it reduces the pressure at the output side of the mixing section and thus reduces the output of the extruder. Also there may be regions in which material may stagnate since the grooves have constant depth in a longitudinal direction. This makes it less suitable for materials of limited thermal stability.

FIG. 2 H shows the Egan mixing section, which has splines that run in a helical direction to form channels separated by mixing barriers. These channels can have a gradually

reducing depth, tapering to zero depth at the end of the mixing section, which reduces the chance of stagnation points. This helical design consumes less pressure than the Maddock style, thus producing less reduction in extruder output.

5 A blister ring, shown in FIG. 2 J, is simply a cylindrical section on the screw that has a small radial clearance, through which all material must pass. This can cause a large pressure drop on the output side of the blister ring, resulting in a significant reduction in overall extruder output.

FIG. 2K reproduces in part Fig. 2 from U.S. Pat. 5,356,208 to *Tadmor*. A portion of the screw surface 33 gradually increases in a radial distance, making a smooth transition to radial maximum at the tip 50. This tip 50 is also rounded and the screw surface 33 then gradually and smoothly decreases in radius to a minimum near the leading wall 58 of a scraping flight 75. The entire cycle from radial minimum through maximum and back to minimum takes place in nearly 180 degree of angular rotation. This increase in the radial distance of the screw surface portion has the necessary effect of decreasing the depth of the screw channel. The volumetric capacity of the screw extruder is decreased when the channels are decreased in depth, thus efficiency of output is reduced. Also, although the *Tadmor* invention may produce some shearing action at the tips, there is no strong elongational flow due to the very gradual reduction in channel depth. As discussed above, elongational stress is much more efficient than shear stress in breaking down agglomerates of material. The

10 15 20 *Tadmor* invention also uses a conventional helix angle of 17-18 degrees. As will be discussed later, the present invention preferably uses a much larger helix angle, which produces much more effective dispersive mixing and much higher output.

Screw extruders can have more than one central screw. Twin-screw extruders may operate with two screws that may either rotate in the same direction, or they may be counter-rotating. There are some machines that use more than two screws.

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In counter-rotating twin-screw extruders, dispersive mixing primarily occurs in the intermeshing region between the screws. This action is similar to that in a two-roll mill. This configuration has the disadvantage that the mixing action creates substantial separating forces on the screws. These forces can push the screws against the barrel, if these forces grow too great. This can cause wear on the screws and the barrel, thus the screw speed has to be kept low, with resulting decrease in the throughput of the extruder.

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In intermeshing co-rotating twin-screw extruders, the screw surfaces in the intermeshing region move in opposite directions. As a result, most of the material bypasses the intermeshing region and moves from one screw to the other repeatedly.

Some twin screw machines have kneading blocks included to increase dispersive mixing. These kneading blocks are most commonly flat paddles of roughly elliptical shape which are stacked on a central shaft, but offset at varying angles. Each paddle on the shaft is paired with a corresponding paddle on the second shaft. The shafts usually both rotate in the same direction but with the angular orientation of the paddles staggered at a certain angle. We can consider the elliptical paddle shapes to have a major and a minor axis with a "tip" on each end of the major axis and a "mid-point" at each end of the minor axis. At one point in the rotation cycle, a tip of a paddle on the first shaft, when horizontally oriented, will nearly contact the midpoint of a paddle on the second shaft, whose tip will then be vertical. As this second, vertical tip rotates towards horizontal, the first tip traces along the elliptical outline of the second paddle, thus "wiping" it. At a further point in the rotation cycle, the second paddle wipes the outline of the first. This wiping action keeps material from stagnating or collecting on the paddle edges. It also imposes constraints on the shapes of the paddles, as the travel of the tip of the neighboring paddle defines the outline of the paddle itself. Although this configuration of paddles can produce fairly good elongational stress in material, the above constraint on the shape of the paddles prevents variations in design, which may produce even better elongational stress regions.

In general, twin-screw extruders are considered to be better at dispersive mixing than single-screw extruders. However for a given capacity, multi-screw machines are usually considerably more costly than single-screw extruders.

For improved mixing to occur, there are several important aspects to be considered. In dispersive mixing, it is the passage of material through a region of high stress that produces the desired breakdown of agglomerates. A single pass through a high stress region will likely achieve only a single rupture of the agglomerate. To achieve a fine scale of dispersion, multiple passes and ruptures may be necessary. Also, for efficient dispersive mixing, stresses in the high stress region should have a strong elongational component, as well as a shear component. For efficient operation of the extruder as a whole, a low pressure drop across the mixing section is desirable. It is also important to combine dispersive and distributive mixing to achieve a more uniform overall mixture. Some distributive mixing occurs whenever dispersive mixing is done, but by deliberately combining distributive

elements with the dispersive elements, chances are improved that all fluid elements will pass through the high stress region, preferably many times, for proper dispersion.

To make sure that all agglomerates and droplets pass through high stress regions at least once, the flow rate through the high stress regions must be large enough compared to the
5 overall forward flow rate. This can be done by designing the number of high stress regions, their length and the size of the gap through which material will pass. It is also preferable that there be more than one high stress region, and that these regions are symmetrically arranged around the circumference of any section along the length of the screw, so that forces will be balanced and the possibility of deflection of the screw will be minimized. To reduce pressure
10 drop in the mixing section, it is desirable to have the high stress regions in a forward helical orientation, which can be done by a continuous forward helix or in a stepped forward helix with kneading disks.

Another consideration which makes improved dispersive mixing desirable, is that as the size of unmelted particles is reduced by better dispersive mixing, these particles are more
15 easily melted. Thus if more efficient dispersive mixing can be generated in the melting zone of the extruder, it can speed up the melting process and the required length of the melting zone can be decreased. This would allow more compact and efficient extruders to be designed.

For the foregoing reasons, there is a great need for a screw extruder which provides
20 better dispersive mixing than in presently available extruders.

DISCLOSURE OF INVENTION

Accordingly, it is an object of the present invention to provide a screw extruder which provides improved dispersive and distributive mixing.

Another object of the present invention is to provide a screw extruder in which
25 material is repeatedly passed through regions of high stress for better break-down of agglomerates into smaller particles.

And, another object of the invention is to provide a screw extruder having a number of high stress regions which produce high elongational stress as well as shear stress.

Yet another object of the invention is to provide a single screw extruder which is less
30 costly to manufacture for its capacity than a multi-screw extruder, but which provides dispersive mixing comparable or better than conventional multi-screw extruders.

A further object of the present invention is to provide a screw extruder in which the high stress regions do not produce a large pressure drop which may impede overall

throughput.

A still further object of the present invention is to provide a screw extruder that has symmetrically balanced high stress regions which avoid possible deflection of the central screw.

- 5 A yet further object of the present invention is to provide a multi-screw extruder that provides improved dispersive mixing over present multi-screw extruders.

An additional object is to provide a screw extruder with modular, exchangeable mixing sections.

- 10 A further additional object is to provide a screw extruder with dispersive mixing elements which can be used in injection and blow molding operations and which provides improved dispersive and distributive mixing.

- 15 Briefly, one preferred embodiment of the present invention is a screw extruder having a barrel which has a bore defining an inner surface and one or more extruder screws, positioned within the bore. The extruder screw or screws include a central shaft and one or more screw flights. The extruder screw or screws further including one or more dispersive mixing elements which interact with the inner surface of the barrel to form one or more progressively narrowing passages through which material is forced into multiple regions of high elongational and shear stress.

- 20 A second preferred embodiment of the present invention is a screw extruder having a barrel, the barrel having a bore defining an inner surface; and one or more extruder screws, positioned within the bore. The extruder screw or screws include a central shaft and a number of dispersive mixing elements which are configured and positioned on the extruder screw or screws to form a number of progressively narrowing passages through which material is forced into multiple regions of high elongational and shear stress.

- 25 Also presented is a method of extruding material using a screw extruder having pushing face profiles that form progressively narrowing passages in conjunction with barrel inner surfaces to provide improved dispersive mixing.

- 30 The described versions of the present invention have many advantages which address the above-mentioned objects. One such advantage of the present invention is that it provides both good dispersive and good distributive mixing.

Another advantage of the invention is that it provides regions of both high elongational and shear stress.

A further advantage of the present invention is that material is repeatedly passed

through regions of high stress for improved breakdown of material agglomerates.

Yet another advantage of the invention is that it may be used in a single-screw extruder, which is less costly for its capacity than a comparable twin screw extruder, yet may provide comparable or better dispersive mixing.

5 A still further advantage of the present invention is that the high stress regions may be in a forward helical orientation, thus reducing pressure drop in the mixing section, and therefore enhancing overall efficiency and throughput.

A yet further advantage of the present invention is that the high stress regions are symmetrically arranged around the central screw, so that deflection is minimized.

10 An additional advantage of the present invention is that the improved dispersive mixing process can enhance melting, so that if dispersive mixing elements are located in the melting zone of an extruder, it can speed up the melting process and reduce the length required for melting the plastic.

A yet further advantage of the present invention is that the dispersive mixing elements
15 can be used in a screw extruder used for injection molding, compression molding and blow molding operations to provide improved dispersive and distributive mixing.

These and other objects and advantages of the present invention will become clear to those skilled in the art in view of the description of the best presently known mode of carrying out the invention and the industrial applicability of the preferred embodiment as
20 described herein and as illustrated in the several figures of the drawings.

BRIEF DESCRIPTION OF THE DRAWINGS

The purposes and advantages of the present invention will be apparent from the following detailed description in conjunction with the appended drawings in which:

FIG. 1 is an overhead view of a simplified screw extruder, in which a portion of the
25 barrel has been cut-away;

FIGS. 2 A-K illustrate a variety of prior art mixing sections for distributive and dispersive mixing;

FIG. 3 shows an isometric view of an extruder screw according to one embodiment of the present invention;

30 FIG. 4 illustrates a cross-sectional view taken through the screw extruder along line A-A in FIG. 1;

FIGS. 5 A-F shows a variety of flight face profiles which embody the present invention;

FIG. 6 illustrates a plan view of a prior art mixing section corresponding to a detailed view of the prior art mixing section seen above in FIG. 2G;

FIG. 7 shows a plan view of an improved mixing section according to an embodiment of the present invention;

5 FIG. 8 is a side view of a screw extruder with a portion of the barrel removed to expose an extruder screw which has been formed according to the present invention;

FIG. 9 is a cross-sectional view taken through the screw extruder along line B-B in FIG. 8;

FIG. 10 shows a perspective view of prior art kneading paddles;

10 FIG. 11 illustrates a perspective view of dispersion disks, which are a preferred embodiment of the present invention;

FIG. 12 shows a perspective view of a screw extruder of which a portion of the barrel has been cut away, including dispersion disks of the present invention;

15 FIG. 13 illustrates a side view of prior art kneading paddles including approach angle α ;

FIG. 14 shows a side view of the dispersion disks of the present invention, including approach angle α ;

FIGS. 15 A & B show front and side plan views of a dispersion disk of the present invention;

20 FIGS. 16 A & B show front and side plan views of a further embodiment of a dispersion disk of the present invention;

FIGS. 17 A & B illustrate front and side plan views of a prior art kneading paddle;

FIGS. 18 A & B show front and side plan views of a modified kneading paddle according to the present invention;

25 FIG. 19 shows a side plan view of a stack of dispersion disks and interleaved transitional elements according to the present invention;

FIG. 20 shows a side plan view of an extruder screw having tapered slots formed in the screw flights according to the present invention;

30 FIG. 21 illustrates a side view of the mixing section of a screw extruder showing both wiping flights and mixing flights according to the present invention;

FIG. 22 shows a close-up detail view of the tapered slot between two flights according to the present invention;

FIG. 23 illustrates a view of an extruder screw, where the cylindrical surface has been

“unrolled” into a flat surface, the view showing a fluted dispersive mixing section according to the present invention;

FIG. 24A-D shows a variety of arrangements of wiping and mixing segments which insure complete wiping as according to the present invention, where the cylindrical surface has again been “unrolled” into a flat surface;

FIG. 25 illustrates a perspective view of an extruder screw where the cylindrical surface has been “unrolled” into a flat surface, the view showing a fluted dispersive mixing section according to the present invention;

FIG. 26 shows a perspective view of another embodiment of a extruder screw where the cylindrical surface has been “unrolled” into a flat surface, the view showing a fluted dispersive mixing section according to the present invention;

FIG. 27 illustrates a perspective view of another embodiment of a extruder screw where the cylindrical surface has been “unrolled” into a flat surface, the view showing a fluted dispersive mixing section according to the present invention;

FIG. 28 shows a perspective view of another embodiment of a extruder screw where the cylindrical surface has been “unrolled” into a flat surface, the view showing a fluted dispersive mixing section according to the present invention;

FIG. 29 illustrates a side view of a mixing section of an extruder screw having semi-circular channels, according to the present invention;

FIG. 30 shows an unrolled view of a mixing section of an extruder screw having semi-circular channels, according to the present invention;

FIG. 31 illustrates a side view of a mixing section of an extruder screw including a number of dispersive mixing elements, according to the present invention;

FIG. 32 shows a side view of a mixing section of an extruder screw including a number of another variation in dispersive mixing elements, according to the present invention;

FIG. 33 illustrates a side cut away view of an extruder screw which is used in an injection molding operation, showing a non-return valve in open valve position, according to the present invention;

FIG. 34 shows a cross-sectional view of the extruder screw taken through line 34-34 in Fig. 33;

FIG. 35 illustrates a side cut away view of an extruder screw which is used in an injection molding operation, showing a non-return valve in closed valve position, according

to the present invention;

FIG. 36 shows a detail cut-away view of a slide ring used with an extruder screw in an injection molding operation; and

FIG. 37 illustrates a front view of the slide ring seen in side view in Fig. 36.

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BEST MODE FOR CARRYING OUT THE INVENTION

A preferred embodiment of the present invention is a screw extruder having improved dispersive mixing. As illustrated in the various drawings herein, and particularly in the view of FIG. 1, a form of this preferred embodiment of the inventive device is depicted by the general reference character 10.

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FIG. 1 illustrates the major portions of a screw extruder 10, having a central longitudinal axis 11, and which also has an input end 12 and an output end 14. Generally, for convenience of reference, the terms "downstream" shall refer to those ends closest to the output portion of the screw extruder and the term "upstream" shall refer to those ends farthest away from the output. The downstream direction is indicated by a large arrow, which shows the direction of material flow. The screw extruder 10 has a barrel 18. The input end 12 includes an input hopper 20 for feeding in material, and an extrusion die 22 on the output end 14. A portion of the barrel 18 has been cut away to show the barrel wall 24, and an inner bore 26. Positioned within the bore 26 is an extrusion screw 28 having screw flights 30.

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Although this version of the preferred embodiment has a single screw, it is to be understood that the screw extruder could contain two or more screws.

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FIG. 2 illustrates a variety of prior art mixing sections of extruder screws, as discussed above in the Background Art section.

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FIG. 3 illustrates an isometric cross-sectional view of one version of a mixing section of an extruder screw 28 used in the present invention. The general reference character 31 designates the mixing section of the extruder screw 28. This mixing section can be an integral portion of the overall screw 28, or it may be a modular section which is combined with other modular sections upon a central shaft to provide varying characteristics which can be customized for different materials and applications. In Fig. 3, an optional central bore 32 is shown in phantom line for the case where mixing section 31 is a modular section which can be stacked upon an independent central shaft. This mixing section is defined as having a length (L) 33. The mixing section 32 includes a central shaft 34 and screw flights 30, which are used to mix the material as well as convey it forward. A screw diameter (D) 35 is defined

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as the tip to tip distance between flights 30 when positioned on opposite sides of the central shaft 34. An arrow is included to indicate the direction of rotation. The flights 30 include the forward pushing face 36, and the rear face 38. Reference character 40 will be used to refer to the cross-sectional profile of the flight 30. As will be seen below, it is the shape of this

5 profile 40 that produces the multiple regions of high elongational and shear stress, which are crucial in producing increased dispersive mixing. In this version of the preferred embodiment, slots 42 have been provided to increase distributive mixing. These slots 42 are optional, and their size and placement are subject to considerable variation, as will be apparent to one skilled in the art. Additionally many other distributive mixing devices may

10 be used, including, but not limited to, pins or protrusions which could be round, square, diamond shape or irregular, secondary flights with interruptions, and changes in channel depth or width (defined below).

FIG. 4 shows a cross-sectional view through the screw extruder 10 along line A – A in Figure 1. Barrel 18 includes the barrel wall 24 surrounding a central bore 26 which is

15 defined by the barrel inner surface 44. In this version of the preferred embodiment, the central bore 26 is cylindrical and accommodates a single extruder screw 28, but it should be understood that the present invention can be used with two or more extruder screws, in which case, the bore 26 cross-section may resemble multiple overlapping circles or ellipses.

The flights 30 of the screw 28 are shown, and in this version of the preferred

20 embodiment there are four flights which are positioned at 90 degree intervals around the circumference of the central shaft 34. It is to be understood that other numbers of flights such as two, three, five, six, etc. may be used, and their positions around the circumference of the shaft 34 is likewise variable. It is desirable, however, that the flights 30 be symmetrically arranged around the shaft 34 circumference in order that the forces on the shaft 34 are

25 balanced and deflection is minimized. The front pushing faces 36 and the rear faces 38 of the flights 30 are shown, as well as the flight profile 40. The front pushing faces 36 and the inner surface of the barrel 44 define a progressively narrowing passage 46 into which the material in the bore 26 moves. The rotational movement of the screw 28 causes the material to enter the large end of the passage 46 and to be squeezed as the passage 46 narrows into high stress

30 regions 48, which are created between the flight tips 50 and the barrel inner surface 44. The reducing cross sectional area of the progressively narrowing passage 46 causes an increase in the average flow velocity. Thus the high stress regions 48 develop both elongational and shear stresses which are important in providing increased dispersive mixing. The action of

the screw 28 rotation ensures that material agglomerates passes through many of these high stress regions 48, and thus very high quality dispersive mixing may be obtained.

The distance between the barrel inner bore 44 and the central shaft 34 will define the channel height (H) 52. The distance between the flight tip 50 and the barrel inner bore 44 is defined as the radial flight clearance (δ) 54. The ratio of the flight clearance 54 to the channel height 52 is defined as δ/H . The distance between the forward pushing face 36 of one flight 30 and the rear face 38 of the next flight 30 on the extruder screw measured circumferentially will be referred to as the channel width 56. Additionally, the width of the tip of the flight (w_f) will be designated as 58, although it is quite possible that this w_f 58 may be zero, depending on the flight face profile 40. Indeed, the profile shown in Fig. 4 is a smooth curve at the tip 50 and thus the flight tip width 58 is zero in this case.

FIG. 5 shows a variety of pushing face profiles 40 of the screw flights 30 which can be used in conjunction with the barrel wall 24 to produce progressively narrowing passages 46 to force material into high stress regions 48. It should be understood that many other variations in profile are possible, and the present invention is not limited to the profiles shown.

The versions of the preferred embodiment discussed so far have had a "positive helix angle" or forward flighted configuration. In a forward flighted screw, the pushing flight face moves the material forward toward the output end of the extruder. Returning to Fig. 1, a positive helix angle (ϕ) 60 can be seen as measured between the face of a screw flight 30 and a vertical reference line 63. It is also possible to have a rearward flighted configuration. In this case, the pushing flight face moves the material backward toward the feed opening of the extruder. It is also possible to have a neutral flight configuration. In this case, the flight angle is ninety degrees, and the pushing flight face moves the material only in the circumferential direction.

In a screw extruder 10, it is possible to have a mixing section that contains a negative helix angle. The sections of the screw which are upstream from the mixing section may still have a positive helix angle in order to make sure that the material is conveyed toward the output end 14 effectively. Thus it should be understood that the present invention 10 may be practiced with variations which include negative helix angles. It is anticipated that the extruder screw 28 may be made to be "modular", having a central shaft upon which mixing sections of varying geometry may be stacked to be adaptable to various materials and operations.

One type of modular mixing section which may be employed is the Maddock mixing section, which was discussed in the background art section and shown in Figure 2 G. FIG. 6 PRIOR ART shows a Maddock mixing section in more detail. The Maddock has longitudinal splines that form a set of semicircular grooves. Alternate grooves are open on the upstream and downstream ends. Material that enters the inlet grooves 70 is forced to pass over the mixing barrier flights 72, which are shown as cross hatched areas, before reaching the outlet grooves 74. While passing over the mixing flights 72, the material is subjected to high shear stress. This can produce some dispersive mixing, but this prior art mixing section only subjects material to a single pass through the high stress region.

In contrast, FIG. 7 shows another preferred embodiment of the present invention in which a multi-flight mixing section 80 can be incorporated in a modular fashion to a screw extruder. Material is introduced through the inlet grooves 70 as before, but must pass over a series of mixing barrier flights 82 before reaching the outlet grooves 74. In passing over this series of flights 82, the material must repeatedly pass through high stress regions.

Additionally, the barrier flights 82 can include a number of progressively narrowing passages 46 to produce regions of high elongational stress 48, thus achieving much better dispersive mixing.

It should be understood that the use of multiple mixing barriers can be used in many different configurations to improve dispersive mixing from that achieved by the prior art. A further example would be to improve the blister ring mixer seen in Fig. 2J of the prior art by using a series of small rings with wedge-shaped leading edges to create multiple high stress regions. Additionally, similar modifications can be made to all fluted mixers such as the Egan, (Fig. 2H), the Zorro, the Troester, etc.

In designing extruder screw mixing sections for good dispersive mixing, there are several variables which can be adjusted to optimize results. According to Tadmor and Manas-Zloczower, (Z. Tadmor and I. Manas-Zloczower, Advances in Polymer Technology, V.3, No.3, 213-221 (1983)), the passage distribution function can be written as:

$$G_k = \frac{\lambda^k e^{-\lambda}}{k!}$$

where k is the number of passes through the clearance, the dimensionless time $\lambda = t_r / \bar{t}$ is the ratio of the residence time t_r and the mean residence time of the control volume \bar{t} . The residence time for a Newtonian fluid can be approximated as follows:

$$t_r = \frac{2z}{v_{bz}(1-r)}$$

where z is the helical length of the screw section considered, v_{bz} the down-channel barrel velocity, and r the throttle ratio (pressure flow rate divided by drag flow rate). The mean residence time can be determined from:

$$\bar{t} = \frac{2WH}{\delta v_{bx} \left(1 + \frac{W}{w_f} \frac{\delta^2}{H^2} \right)}$$

where W is the channel width, H the channel depth, δ the radial flight clearance, and w_f the flight width. The dimensionless time can be written as:

$$\lambda = \frac{L\delta \left(1 + \frac{W}{w_f} \frac{\delta^2}{H^2} \right)}{WH(1-r)\cos\phi}$$

where L is the axial length corresponding to down-channel distance z . The fraction of the fluid experiencing zero passes through the clearance is:

$$G_0 = e^{-\lambda}$$

The G_0 fraction should be low to make sure that most of the fluid experiences at least one or more passes through the clearance. In a simple conveying screw the G_0 fraction is usually around 0.9, which means that most of the fluid passes through the extruder without ever passing through the clearance. The expressions above can be used to determine the minimum value that will yield a G_0 less than 0.01, meaning that less than one percent of the fluid will not pass through the clearance at all. This is achieved when the dimensionless time $\lambda > 4.6$. For certain values of L , H , W , r , ϕ , w_f we can then determine how large the flight clearance δ has to be to make $\lambda > 4.6$ or $G_0 < 0.01$.

When $L=3W$, $r=0$, and $\phi=17.67^\circ$, the ratio of δ/H has to be about 0.8 to achieve a $G_0 < 0.01$. Clearly, with such a high ratio of δ/H it will be almost impossible to create large stresses in the clearance and to accomplish effective dispersive mixing. From equation 4 it is clear what geometrical variables we have to change to achieve a low G_0 fraction at a small clearance. We can do this by 1) increasing L , the length of the mixing section, 2) increasing ϕ , the helix angle, 3) reducing w_f , the width of the flight, and 4) increasing the number of flights.

If the helix angle is increased from 17.67 to 60 degrees with the other values being the same, the δ/H ratio has to be about 0.35 or greater for the G_0 fraction to be less than 0.01.

This value is still rather larger, but substantially better than 0.8. The δ/H ratio can be further reduced by increasing the length of the mixing section or reducing the flight width or by

5 increasing the helix angle even more. This procedure allows a first order determination of the design variables. Further refinement of the initial values can be obtained from computer simulation.

It is estimated that in prior art screw extruders with a simple conveying screw, G_0 , the fraction of material that does not pass through the clearance, is typically 0.9. This means that
10 a great deal of material never passes through high stress regions, and thus dispersive mixing is poor.

In the present invention, it is desired that G_0 is less than 0.01, and therefore greater than 99% of the material will pass through a region of high stress. It is anticipated from the above formulas that for this value of G_0 , in order to achieve a δ/H ratio in a reasonable range
15 of 0.05 to 0.3, the helix angle (ϕ) will lie in the range of -90° to -30° and $+30^\circ$ to $+90^\circ$, the length of the mixing section (L) will lie in the range of 1 to 20 times the bore diameter, and the width of the screw flight at the tip (w_f) will lie in the range of 0 to 0.5 times the diameter, D .

It should be understood that although the preferred range of helix angles is -90° to -30° and $+30^\circ$ to $+90^\circ$, values in the range from $+30^\circ$ to -30° will work as well.
20

Multiple passes through a high stress region are necessary to break down agglomerates. Thus even in mixing sections with very low values for G_0 , there is no assurance that good dispersive mixing will be achieved. For example, in the Maddock prior art mixer, all the material has to pass through the high stress region, but it only passes
25 through this region once, which is insufficient.

Another parameter of interest is the ratio of flight clearance to the screw diameter or δ/D . This gives an indicator of how much material flows through the high stress regions, and thus is proportional to how well the material is dispersively mixed. The higher this number is, the better the dispersion can be expected. For prior art single screw extruders, this δ/D
30 figure is typically 0.001, and for prior art twin screw extruders, this δ/D figure improves to 0.005. In contrast, the δ/D value for the various preferred embodiments of the present invention is 0.005 to 0.250. When the δ/D number becomes too high the stresses that will be generated may be too low to accomplish dispersive mixing. The clearance should be small

enough to be able to generate high enough stresses but large enough to allow sufficient material to flow through it.

The flights of a screw extruder can convey material in the downstream direction and can also serve to prevent material from building up on the walls of the extruder barrel. This latter function is known as "wiping" and it is possible to have elements that perform this wiping separately from the function of conveying material, although typically the functions are combined. It is also possible that wiping and conveying can be performed by one set of screw flights, while mixing is done by a second set of flights. This second set of flights may be in a separate modular section, or in the same section by incorporating this second set of flights between the conveying/wiping flights. The mixing flights do not have to have the same helix angle as the conveying/wiping flights, and indeed it may be beneficial that they be different. The helix angle of the conveying flights can be chosen to give the best pumping action, while the helix angle for the mixing flights can be chosen to give the best dispersive mixing action. A functional separation of the two types of flights can thus be achieved, allowing optimization of the overall performance.

FIG. 8 show a screw extruder 90 with a modified central screw 92 in which the mixing flights 94 are included between the conveying/wiping flights 96.

FIG. 9 is a cross-sectional view of Fig. 8 taken through line B – B. The profile 40 of the mixing flights 94 can be seen to produce a progressively narrowing passage 46 in the barrel 18 which again forces material into regions of high stress 48. This configuration causes enhanced material dispersion while the wiping/conveying flight 96 has been designed for optimal pumping characteristics.

As mentioned above, it is also possible to have a variation in which the helix angle is ninety degrees. This is accomplished by using straight disks which are offset from each other at varying rotational angles. For a single screw extruder, this version of the preferred embodiment is similar to kneading paddles used in twin screw extruders, but with the important difference and advantage that the geometry of the disks can be optimized for production of effective elongational and shear stress, rather than being constrained by the need to trace the outline of a second screw.

FIG. 10 Prior Art shows the configuration of the kneading paddles in one screw of a twin screw extruder as in the prior art. In contrast, FIG. 11 illustrates a second preferred embodiment 100 of the present invention for use in a single screw extruder having dispersion disks 102 aligned upon a central longitudinal axis 104. The pushing flight faces 106 have a

pronounced wedge shape, and the trailing flight face 108 is flat. Stagger angle β 109 is shows the rotational offset of the successive disks. In a similar manner to that discussed above in regard to the profile of the pushing flight faces 30 in the positive helix angle embodiment, the profiles of the pushing faces 106 of the dispersion disks 102 are capable of much variation, such as elliptical sections, triangles, circular sections, etc. Additionally, these dispersion disks 102 may also be modular, and may be stacked upon a central shaft to provide various mixing characteristics.

FIG. 12 shows such a version of the preferred embodiment 100 in which dispersion disks 102 having a ninety degree helix angle have been fixedly stacked upon a central shaft 110. A portion of the barrel 118 has been cut away to show the orientation of the disks 102. A central longitudinal axis 104 has again been included for easy reference. Elongational and shear stress necessary for good dispersive mixing are produced in the high stress regions 120 between the paddle tips 122 and the barrel inner surface 124. The main dispersive mixing action will occur in the narrowing region formed by the pushing flight face 106 and the inner barrel surface 124. Material is forced into the progressively narrowing passage 126 by drag flow caused by the relative motion between the screw and the barrel surface 124.

FIG. 13 PRIOR ART and FIG. 14 show a comparison of the profiles of the prior art and the dispersion disks of the present invention. In Fig. 13, a prior art kneading paddle in a barrel of a screw extruder is illustrated with line 128 drawn tangent to the surface of the paddle at the tip. A second line 130 is drawn tangent to the point on the barrel's inner surface which intersects the projection of line 128. The two lines 128 and 130 define an angle α which is designated as 132. The geometry of the kneading paddle is constrained by the necessity of mating with a second paddle whereby the tip of the first paddle wipes the second and thereby traces the required contour. Angle α 132, which defines the entrance angle to the passage past the tip, is severely limited by this design constraint, and is not optimized for dispersion of material.

In contrast, the profile of a preferred embodiment of present invention 100 is shown in Figure 14. A dispersion disk 102 is illustrated in the bore 124 of a screw extruder 10. A line 134 is shown tangent to the disk's surface near the tip 122. As before, a second line 136, tangent to the projected point on the barrel's inner surface 124, defines an angle α 138. Since the geometry of the dispersion disk 102 is not dictated by the necessity to trace the outline of an adjacent paddle, the angle α 138 can be much more acute and can be designed to produce excellent dispersion of the material. It is anticipated that this angle α 138 will lie in the range

of zero to 35° , while the typical angle α 132 found in prior art kneading paddles from twin screw extruders is 35° to 50° . By way of comparison, this corresponding approach angle α in prior art single screw extruders is typically 90° , since there is no progressively narrowing passage provided.

5 While the material is forced all the way into a progressively narrowing passage, and through it, dispersive mixing action will be efficient. However, the polymer melt will have a tendency to bypass the high stress regions and take the path of least resistance by flowing around them as can be seen in FIG. 15 A & B. In Fig. 15 A, a dispersion disk 102 is seen in profile as well as a small portion of the barrel's inner surface 124. The high stress region 120
10 is shown between the disk tip 122 and the barrel's inner surface 124. Fig. 15 B shows a front plan view of the same dispersion disk 102 with flow of material 140. Material 142 is shown flowing around the sides of the disk tip 122. This will reduce the efficiency of the dispersive mixing action.

This problem can be greatly reduced by the addition of a barrier wall in the high stress
15 region to close off the bypass route. FIGS. 16 A & B show another preferred embodiment 150 of the present invention in which two barrier walls 154 have been added. Fig. 16A shows a side plan view of the modified dispersion disk 152 with barriers 154 at the tips 122. Fig. 16B shows a front plan view of the modified dispersion disk 152 with material flow 140 which is channeled through the high stress region 120. The efficiency of the dispersive
20 mixing is thus enhanced.

This modification can also be used with prior art kneading paddles to improve performance as seen in FIGS. 17 A & B and 18 A & B. Fig. 17 A & B show side and front plan views of a prior art kneading paddle without modifications. Fig. 18 A shows a side plan view of a modified kneading paddle 160 which has been improved by means of the present
25 invention. A groove 162, seen in dashed line in Fig. 18 A, has been cut into the surface of the paddle 160. Fig. 18 B shows a front plan view of the modified paddle 160 with the groove 162 included. This groove 162 can channel material into the region between the tip 164 and the barrel wall 124. Although the paddle's shape is still largely dictated by the tracing of its companion paddle, the region in the groove 162 can be angled differently to improve material
30 dispersion. This is expected to produce improved performance, although it may not reach the efficiency of the dispersion disks 102.

There is a common problem which exists in regard to mixing elements which have a neutral helix angle, such as both kneading paddles and dispersion disks. This problem is that

there may be stagnation points which exist at the transition between the different disks. This condition can be corrected by the use of transition elements between the straight disks. FIG. 19 illustrates one form that transitional elements might take. Dispersion disks 102 are interleaved with one or more transition elements 166. In this version of the preferred
5 embodiment, the transition elements are flighted elements with a helix angle between zero and 90° . These elements 166 may be basically shaped as twisted dispersion disks with the angle of twist equal to the stagger angle 109 (see Fig. 11) of the dispersion disks 102. Transition elements flights 168 are shown connecting the tips 122 of the disks 102. These elements provide a gradual transition from one dispersion disk to another and aid the flow of
10 material while still maintaining the dispersive mixing capability. It is to be understood that these transition disks may also be used with kneading paddles of the prior art to improve material flow.

It should be further understood that the improvements of the present invention can be used in screw extruders that contain multiple screws. Twin-screw extruders can be co-
15 rotating with screws rotating in the same direction, or counter-rotating with screws rotating in the opposite direction. There are also triple-screw extruders, quadruple-screw extruders, and screw extruders with ten screws arranged in a circular pattern. All varieties of screw extruders can benefit from improved dispersive mixing by using the preferred embodiments of the present invention which are presented above. Increasing the number of high stress
20 regions by using flights with the profiles shown above, is a technique that can be useful in any of multiple as well as single screw extruders. Therefore, in addition to the above mentioned examples, various other modifications and alterations of the inventive device/process 10 may be made without departing from the invention.

Another variation of extruder screw geometry having different dispersive mixing
25 elements is shown in FIG. 20. This extrusion screw 200 has a number of screw flights 202, each flight having a mixing portion 204 and a wiping portion 206. The flights 202 are interrupted by slots 208 which improve not only distributive mixing, but which are tapered to improve dispersive mixing as well. The slots 208 have a taper angle 210, which is preferably in the range of 20 to 60 degrees. The tapering of the slots 208 provide narrowing channels
30 212, which once again create multiple regions of high elongational stress 214.

Two other angles of interest are the slot pushing flank angle 216 and the slot trailing flank angle 218, which are shown in FIGS. 20, 21 and 22. These angles are measured in a clockwise rotation from a vertical reference. In Fig. 20, the trailing flank angle 218 is equal

to zero degrees, while in Figs. 21 and 22, this is a non-zero angle. Fig. 22 shows a detail view of two adjacent wiping flight portions 206, wherein the importance of this non-zero slot trailing flank angle 218 can be seen more easily. The solid outline of the non-shaded area defines a slot trailing flank 220 which has a zero angle. As the screw rotates, there remains a region 222, which is not wiped by the flight 206, assuming that there is not another wiping flank whose travel overlaps this region. However, if the shaded area in the dashed outline 224 is added to the wiping flight 206, the slot trailing flank angle 218 is large enough (in this case, about 35 degrees) that the region 222 is wiped in the course of the screw rotation. Although this slot trailing flank angle 218 has been increased, the slot 208 still tapers as shown by taper angle 210, thus producing effective dispersive mixing. This configuration of wiping flights which have a tapering slot but no regions which are left unwiped in the course of screw rotation will be referred to as "fully wiping flights" 226.

The trailing slot flank angle that is required to achieve full wiping depends on the width of the slot, the thickness of the flights and the helix angle of the screw flights. It is also possible that the wiping flight segments may overlap in their path of travel, thus making the angle of the slot trailing face less important.

Another feature which is apparent from Fig. 21 is that a flight segment 228, which is defined as a portion of the screw flight 202 bounded at the ends by slots 208, can be entirely of a mixing portion 204 or entirely of a wiping portion 206. Fig. 21 shows segments which are entirely of a mixing character to make mixing segments 234, and segments which are entirely of a wiping nature to form wiping segments 236. Indeed, for ease of manufacture, this separation of portions into discrete segments is very desirable. It is to be understood that any combination of mixing portions and wiping portions is possible, whether combined onto one segment or separated into different segments. All of these combinations are to be considered included in the scope of this invention.

For an example, a mixing section can be designed that has wiping segments 236, without any mixing segments, but with tapered slots 208 between the segments 236. The flight 202 composed of these wiping segments 236 may be a fully wiping flight 226, but is not necessarily so. Dispersive mixing in this case would then be achieved solely by the elongational flow generated in the tapered slots 208. Even without any segments having mixing portions, significant improvement in mixing performance is created. Especially when modular mixing segments are stacked upon a central shaft, as discussed above, the relative lengths and numbers of the mixing segments 234 and the wiping segments 236 can be easily

changed, depending on whether more wiping or mixing is desired.

FIG. 23 shows a four flighted mixing screw with angles and dimensions which have been found to be especially efficient in operation. This figure presents an "unrolled view", which simulates the pattern made by the screw flights if they were rolled onto a flat surface.

5 Thus dimension 238 corresponds to the circumference or a measurement of πD where D is the diameter of the screw. Wiping flight segments 236 are shown in black, and mixing flight segments 234 are shown in white. It is to be understood that many other combinations of angles and dimensions are contemplated by the present invention, as long as the tapered slots are used to provide improved dispersive mixing. Also, the number of flights is not limited to
10 four.

The helix angle ϕ 60 is shown as measured from a vertical reference line 63. A preferred range of angles for the helix angle ϕ 60 is between 20-90 degrees, the slot pushing flank angle 216 preferably is in the range of 0-90 degrees, the slot trailing flank angle 218 preferably is in the range of 0-50 degrees, the slot width preferably is in the range of 0.02-
15 0.25D, and the flight width preferably is in the range of 0-0.5D.

One preferred example of a configuration of these variables which lie in these ranges is seen in Fig. 23. Here, the helix angle ϕ 60 is 45°, the slot pushing flank angle 216 is also 45°, and slot trailing flank angle 218 is 20°. The slot width 240 is approximately 0.05D and the flight widths are approximately 0.10D. This configuration allows for slot taper angles
20 210 of approximately 25°, and due to the non-zero slot trailing flank angle 218, all four flights are fully wiping flights.

It is desirable that the entire circumference of the barrel be fully wiped in order to prevent material build-up and impediments to flow. FIGS. 24 A-D illustrate various
25 arrangements of wiping segments 236 and mixing segments 234 which insure complete wiping. Once again, the figures are shown in unrolled view. For ease of drawing in the scale presented, the taper angles of the slots are not shown in these figures, but it is to be understood that the slots are indeed tapered, and the flights are fully wiping flights. The dark segments depict the wiping segments 236, while the mixing segments 234 are white. Fig. 24A shows a configuration where every flight 202 is composed of one wiping segment 236 to
30 three mixing segments 234. This is referred to as "every flight is 1/4 wiped". By the same nomenclature, Fig. 24B shows every other flight is 1/2 wiped, Fig. 24C shows one flight completely wiped, and Fig. 24D shows two flights 1/6 wiped and two flights 1/3 wiped.

A new type of fluted mixing section 300 including another type of dispersive mixing element is illustrated, again in "unrolled view", in FIG. 25. In this variation, the shaft portion 304 of the screw 302 is provided with ramp sections 306 which act in conjunction with mixing flight sections 308 to provide multiple regions of elongational stress 310. The ramp sections 306 provide a series of crests 312 and troughs 314. The approach to the crests 312 provide regions of increased pressure and elongational stress which are bounded on the upstream side by a main flight section 316 which, along with the mixing flight sections 308, serve to define a channel 318. The main flight sections 316 are designed to maintain the material in the channel 318, and convey the material downstream. The downstream side is bounded by a mixing flight 308 which has a narrowing profile 320, and may containing mixing grooves 322 or other distributive mixing elements. As the material is forced up the ramp 306, it therefore either passes through the high stress region 310 at the crest 312, or flows over the mixing flight section 308 into a region of relatively lower pressure at an adjacent trough 314. In either case, dispersive mixing is enhanced by the passage of material through multiple regions of elongational stress 310.

Generally, within the fluted mixing section 300, a number of dispersive regions 330 are formed. Each dispersive region 330 has at least one inlet portion 332, and at least one outlet portion 334. The dispersive regions 330 are configured so that material must pass through a high stress region 310 as it leaves the outlet portion 334 of the dispersive region 330, and each outlet portion 334 connects to the inlet portion 332 of an adjacent dispersive region 330. This guarantees that material must pass through multiple regions of high stress thus causing more effective dispersive mixing.

In this embodiment, the inlet portion 332 of the dispersive region 330 corresponds to the troughs 314, and the outlet portions 334 are formed by the crests 312, as well as the mixing flights 308 over which the material must pass before reaching the next trough 314. It should be noted that both types of outlet portions 334, the crests 312 and mixing flights 308 have the same type of narrowing profile which produces the regions of high elongational stress which provide improved dispersive mixing.

The screw 302 illustrated is configured with the crest of an upward ramp abutting the crest of the next downward ramp and the trough of that ramp abutting the trough of the next upward ramp. However, it is to be understood that a screw could be configured so that the crest of one ramp abuts the trough of the next ramp, or in other words, there could be a series of upward ramps, or alternately, downward ramps. Of course, it will be apparent to those

skilled in the art that any combination of upward and downward ramps may be used, and the combinations produced may be tailored to requirements of the extrusion materials.

A further variation in the fluted mixing section 400 with dispersive mixing regions is shown in FIG. 26, also in "unrolled view". The shaft 404 in this variation is configured with
5 a number of main flights 416, which serve to confine the flow of material to channels 418 therebetween. Within these channels 418 are a number of wedge-shaped barrier flights 408 which serve to create regions of elongational stress 410 as the material is forced up the triangular ramp 406 of the flights 408. The flights 408 have a drop face 424 over which the material must flow to escape the high pressure region, and this drop face 424 may be
10 configured with distributive regions 422 such as teeth or mixing grooves to further mix the material.

Again, the channels 418 can be considered to be made up of a number of dispersive regions 430, each having at least one inlet portion 432, and at least one outlet portion 434. Material must pass through a high stress region 410 as it leaves an outlet portion 434 of the
15 dispersive region 430, and each outlet portion 434 connects to the inlet portion 432 of an adjacent dispersive region 430. As before, this guarantees that material must pass through multiple regions of high stress thus causing more effective dispersive mixing.

The fluted mixer 400 shown in Fig. 26 has three such barrier regions 408 thus providing three passes through a high stress region 410, but of course the number of barrier
20 regions included is subject to much variation and not limited to three.

FIG. 27, another "unrolled view", shows a yet further variation, designated as fluted mixing section 500, which again uses a number of main flights 516 on the shaft 504 to create channels 518 in which material flows. A number of wedge-shaped barrier flights 508 again act to create regions of high stress 510 before the material flows down the drop faces 524,
25 which again may be configured with distributive elements 522. Again, dispersive regions 530 may be identified having at least one inlet portion 532 and at least one outlet portion 534.

FIG. 28 shows a variation of the embodiment of Fig. 27, in which additional triangular ramp elements 520 have been added to the barrier flights 508 to avoid the creation of stagnation points, where material may otherwise accumulate. The channel 518 is shown
30 from the upstream end in order to illustrate the features more clearly.

As before, the channels 518 seen in Figs. 27 and 28 can be considered to be composed of a number of regions 530, each of which has at least one inlet portion 532, and at least one outlet portion 534. The dispersive regions 530 are configured so that material must pass

through a high stress region 510 as it leaves the outlet portion 534 of the dispersive region 530, and each outlet portion 534 connects to the inlet portion 532 of an adjacent dispersive region 530. This guarantees that material must pass through multiple regions of high stress thus causing more effective dispersive mixing.

5 Much the same principle works in the embodiment shown in FIGS. 29 and 30. Fig. 29 shows a side view of an extruder screw mixing section 550, while Fig. 30 illustrates an unrolled view of the same mixing section 550. Referring now to both figures, the shaft 552 has a diameter just slightly smaller than the diameter of the barrel (not shown). Into this shaft are machined a number of semi-circular channels 554, preferably created by ball milling.

10 Since the unmilled portion of the shaft 552 fills the barrel except for enough clearance to allow for rotation, these unmilled portions act as barrier flights 556 to direct the flow of material. A number of these flights, shown in cross-hatch, are then machined to create mixing flights 558 each of which have a narrowing profile between a channels' 554 outlet portion 560 and the inlet portion 562 of a neighboring channel 554. This provides multiple

15 regions 564 of high elongational and shear stress, as before. Arrows show representative flow paths of material, by which it can be seen that material must pass through many of these regions 564 of high stress before leaving the mixing section, thus insuring excellent dispersive mixing. The mixing flights 558 can of course include other mixing elements such as pins, grooves, etc.

20 An advantage of this embodiment is the ease with which it can be manufactured, since ball milling is a well-known and relatively inexpensive method of manufacture.

FIG. 31 illustrates a side view of an extruder screw 600, which has another variety of dispersive elements. A central shaft 602 has a number of dispersive elements 604, which, in this embodiment, are roughly diamond shaped pins or protrusions. The shape and position of

25 these elements 604 on the shaft 602 again create gradually narrowing passages 606, which create multiple regions 608 of high elongational and shear stress.

FIG. 32 illustrates another variation of this concept. A side view of a extruder screw 600 is shown in which dispersive elements 610 are pins or protrusions which have a triangular profile. Again, narrowing passages 606 create multiple high stress regions 608.

30 This arrangement has the advantage that the dispersive elements are arranged in a helical configuration, which can reduce the pressure drop across this region.

It is to be understood that many variations of this arrangement could be used, which would be obvious to one skilled in the art. Many other types of polygons or non-polygons

could be used as the dispersive elements. If triangular elements are to be used, they could be of many different types such as isosceles triangles, right triangles, etc. and the triangles could assume many different positions and orientations on the shaft, as long as they form the required narrowing passages for high elongational and shear stress. All such variations are within the scope of the present invention.

The dispersive elements described and pictured may also be used in injection molding machines. The mechanisms used in these machines are also sometimes called "plasticating units". However, these plasticating units may be so similar in structure to the mechanisms in regular screw extruders that for the purposes of this application, the term "screw extruder" shall be understood to include both injection molding machines and other types of molding machines such as blow molding machines, compression molding machines, etc. Effective dispersive mixing is important to all these types of machines. Thus the creation of multiple progressively narrowing passages which form regions of high elongational and shear stress such as are provided by the present invention is an very valuable improvement to any machine of this type.

FIG. 33 shows a screw extruder 700 which is being used in an injection molding operation. The injection molding machine is shown in an "open valve" position, which will be described below. The arrows included show the direction of material flow and point in a downstream direction. As before, the screw extruder 700 includes an extruder screw 701 which includes a number of screw flights 702. The screw 701 includes a central shaft 706 upon which two slotted rings are mounted. A slide ring 708 (shown in cut-away view) is free to move in an axial direction along the shaft's longitudinal axis 712. A stationary ring 710 is fixed to the shaft 706 and rotates as the shaft rotates and is thus "stationary" with reference to this shaft. The stationary ring 710 includes a number of dispersive mixing elements 714. As in the other embodiments previously described, the dispersive elements 714 are shaped and positioned upon the screw 701 to produce gradually narrowing passages 716 which, again, produce multiple regions of elongational and shear stress 718. It will be obvious to one skilled in the art that there may be two or more stationary rings on the shaft, and that these rings may be in the form of modular sections which can be stacked upon the central shaft.

Although not visible in this view, the inner circumference of the slide ring 708 is also formed with dispersive elements, which will be discussed below. The chamber where the injection material is mixed and plasticized is referred to as the plasticizing chamber 720. In Fig. 33, it includes the area within the barrel 704 in the downstream direction from the shaft

shoulder 722

The injection molding operation demands that appropriate pressure be generated within the barrel 704 and that injection material be well plasticized before being injected into the mold. To accomplish these purposes, nearly all injection molding machines include a non-return valve, which, when open, allows material to enter the plasticizing chamber, but when closed prevents material from exiting the plasticizing chamber, and allows pressure to build in the chamber. In the present invention, the non-return valve is an assembly formed from the shaft shoulder 722 and the upstream shoulder 724 of the slide ring 708. The non-return valve assembly shall be indicated by the number 726.

When the non-return valve 726 is in open position, the mold (not shown) is closed. The screw 701 rotates and moves backwards in the barrel 704. Material then flows into the plasticizing chamber 720 as indicated by the arrows. The material passes through the dispersive elements on the inner circumference of the slide ring (see also Fig. 34) and then through the dispersive elements 714 on the stationary ring 710, and are mixed as the screw 701 turns.

FIG. 34 shows a cross-sectional view of the screw extruder 700 as taken through line 34-34 in Fig. 33, including the barrel 704, and the stationary ring 710 with the dispersive mixing elements 714.

FIG. 35 illustrates a side cut-away view of a screw extruder 700 used in an injection molding operation in which the non-return valve is now in the "closed valve" position. The screw 701 has now moved forward in the barrel 704 so that the shaft shoulder 722 contacts the upstream shoulder 724 of the slide ring 708, thus closing the non-return valve 726. The plastic melt can now be pushed into the mold without material leaking backwards.

FIG. 36 shows a detail cross-sectional view of the slide ring 708 showing the dispersive mixing elements 714 on the inner circumference of the ring 708. The narrowing passage 716 and the high stress regions 718 are also shown.

FIG. 37 illustrates a front view of the slide ring 708 seen in side view in Fig. 36. The dispersive elements 714 and the high stress regions 718 are shown.

Therefore, in addition to the above mentioned examples, various other modifications and alterations of the inventive device/process 10 may be made without departing from the invention. Accordingly, the above disclosure is not to be considered as limiting and the appended claims are to be interpreted as encompassing the true spirit and the entire scope of the invention.

INDUSTRIAL APPLICABILITY

The present screw extruder 10 is well suited generally for application in any mixing process where a solid or liquid ingredient needs to be mixed dispersively in a viscous fluid. This may be the dispersion of solid agglomerates in a viscous fluid or the dispersion of liquid droplets in a viscous fluid. It is particularly well suited for use in mixing blends of polymers or for mixing additives to polymers prior to extrusion forming.

Applications in the polymer field include the dispersion of solid pigments into polymers for making colored plastic products. Particularly where uniformity of color is important, it is very advantageous that the color particles be well mixed dispersively and broken down into smaller agglomerates than may be possible through merely distributive mixing.

The present invention 10 can also be used to improve the dispersion of incompatible polymer components into a polymer matrix to produce polymer blends and alloys. Good dispersive mixing can be important in obtaining uniform material properties such as tensile strength, durability, etc. Reinforcing fillers can be added to a polymer matrix to produce increased stiffness with greater uniformity using the present invention 10.

When manufacturing conductive or semi-conductive materials, the dispersion of conductive fillers in a polymer matrix is enhanced by use of the present invention 10. The dispersion of magnetic fillers in plastic magnets, and dispersion of solid fillers for increased resistance to oxidation can both be improved when using the improved dispersive mixer 10. The present invention 10 is also useful in the manufacture of rubber adhesives.

The viscous fluid to be dispersively mixed does not have to be plastic or polymer based. It is possible to mix food products such as dough, mashed potatoes, cooking oil, a slurry of grapes or fruit concentrates, honey or peanut butter. It can also be petroleum products like oil or rocket fuel, etc. All of these materials may benefit from the improved dispersive mixing which is provided by the present invention 10.

Additionally, since the mixing elements of the present invention can be made to be modular, it is possible to customize configurations for optimum performance with a particular material. The improvements of the present invention 10 may thus also be incorporated into existing screw extruders at reduced cost. Particularly, improvements to prior art kneading paddles may be made by using conventional machining methods to include the improved dispersive groove 162 in existing machines for little cost. For even better performance, dispersion disks 102, which may be manufactured to the same diameter and standard shaft

fitting dimensions as the prior art paddles, may replace the kneading paddles.

Another consideration which makes improved dispersive mixing desirable, is that as the size of unmelted particles is reduced by better dispersive mixing, these particles are more easily melted. Thus if more efficient dispersive mixing can be generated in the melting zone of the extruder 10, it can speed up the melting process and the required length of the melting zone can be decreased. This would allow more compact and efficient extruders to be designed. Factory floor space could be reduced at great savings. Also, as the melting process is increased, overall throughput of the extruder 10 is increased, resulting in an increase in overall efficiency, with attendant cost savings.

The screw extruder 700 having dispersive mixing elements 714 which are positioned to form progressively narrowing passages 716 is also useful in injection molding, blow molding, compression molding and other kinds of molding operations.

For the above, and other, reasons, it is expected that the screw extruder 10 of the present invention will have widespread industrial applicability. Therefore, it is expected that the commercial utility of the present invention will be extensive and long lasting.

IN THE CLAIMS

What is claimed is:

- 1 1. A screw extruder comprising:
2 a barrel, said barrel having a bore defining an inner surface; and
3 at least one extruder screw, positioned within said bore, said at least one
4 extruder screw including a central shaft and at least one screw flight, said at least one
5 extruder screw further including at least one dispersive mixing element which
6 interacts with said inner surface of said barrel to form at least one progressively
7 narrowing passage through which material is forced into at least one region of high
8 elongational and shear stress.
- 1 2. The screw extruder of claim 1 wherein:
2 said at least one dispersive mixing element includes at least one tapered slot formed in
3 said at least one screw flight, said at least one tapered slot forming at least one progressively
4 narrowing passage through which material is forced into at least one region of high
5 elongational and shear stress.
- 1 3. The screw extruder of claim 2 wherein:
2 said at least one tapered slot has a taper angle which is in the range of 20 to 60
3 degrees.
- 1 4. The screw extruder of claim 1 wherein:
2 said at least one flight includes a mixing portion and a wiping portion.
- 1 5. The screw extruder of claim 1 wherein:
2 said at least one flight includes discrete mixing segments and wiping
3 segments.
- 1 6. The screw extruder of claim 1 wherein:
2 said at least one flight has only wiping segments.

- 1 7. The screw extruder of claim 2 wherein:
2 said at least one flight includes at least one non-zero slot pushing flank angle.
- 1 8. The screw extruder of claim 2 wherein:
2 said at least one flight includes at least one non-zero slot trailing flank angle.
- 1 9. The screw extruder of claim 1 wherein:
2 said at least one flight is a fully wiping flight.
- 1 10. The screw extruder of claim 2 wherein:
2 said extruder screw has a Diameter dimension;
3 said flight has a helix angle, a slot trailing flank angle, a slot pushing flank
4 angle, a slot width and a flight width;
5 said helix angle is in the range of 20-90 degrees;
6 said slot pushing flank angle is in the range of 0-90 degrees;
7 said slot trailing flank angle is the range of 0-50 degrees;
8 said slot width is in the range 0.02-0.25 Diameters; and
9 said flight width is in the range of 0.0-0.5 Diameters.
- 1 11. The screw extruder of claim 5 wherein:
2 said screw extruder has four flights which are arranged in a flight segment
3 configuration, which is a variable to be selected from a group consisting of every
4 flight 1/4 wiped, every other flight 1/2 wiped, one flight is completely wiped, and two
5 flights 1/6 wiped and two flights 1/3 wiped and every flight 1/3 wiped except for the
6 fourth flight.
- 1 12. The screw extruder of claim 1 wherein:
2 said at least one dispersive mixing element include at least one fluted mixing
3 section;
4 each said fluted mixing section having a plurality of adjacent dispersive
5 regions;
6 each of said adjacent dispersive regions including at least one inlet portion and
7 at least one outlet portion, and at least one region of high elongational and shear

8 stress; and
9 said adjacent dispersive regions being configured so that an outlet portion of
10 one adjacent dispersive region directs material into an inlet portion of another
11 adjacent dispersive region so that material is forced through multiple regions of high
12 elongational and shear stress.

1 13. A screw extruder as in claim 12 wherein:
2 said adjacent dispersive regions of said fluted mixing section include a
3 plurality of barrier flights which create multiple regions of high elongational and
4 shear stress.

1 14. A screw extruder as in claim 13 wherein:
2 said barrier flights include ramps which are formed on said central shaft of
3 said extruder screw.

1 15. A screw extruder as in claim 14 wherein:
2 each of said ramps has a crest and a trough, said ramps being arranged crest to
3 crest and trough to trough.

1 16. A screw extruder as in claim 14 wherein:
2 each of said ramps has a crest and a trough, said ramps being arranged crest to
3 trough.

1 17. The screw extruder of claim 13 wherein:
2 said barrier flights are bounded by main flight sections and mixing flight
3 sections.

1 18. The screw extruder of claim 17 wherein:
2 said mixing flight sections are formed with wedge-shaped profiles to further
3 create regions of high elongational and shear stress.

1 19. The screw extruder of claim 17 wherein:
2 said mixing flights include distributive mixing elements.

- 1 20. The screw extruder of claim 13 wherein:
2 said barrier flights of said fluted mixing section include a plurality of
3 triangular wedge shapes which are formed on said central shaft.
- 1 21. The screw extruder of claim 13 wherein:
2 said barrier flights include distributive mixing elements.
- 1 22. The screw extruder of claim 12 wherein:
2 said fluted mixing section includes a plurality of semi-circular channels.
- 1 23. The screw extruder of claim 1 wherein:
2 said at least one extruder screw is a pair of twin extruder screws.
- 1 24. The screw extruder of claim 23 wherein:
2 said twin extruder screws rotate in counter directions.
- 1 25. The screw extruder of claim 23 wherein:
2 said twin extruder screws rotate in the same direction.
- 1 26. The screw extruder of claim 1 wherein:
2 said at least one extruder screw includes modular sections which can be
3 arranged on a central shaft to provide variable mixing characteristics.
- 1 27. The screw extruder of claim 1 wherein:
2 said at least one screw flight is a plurality of screw flights which are
3 symmetrically arranged about a central shaft to balance deflection forces.
- 1 28. The screw extruder of claim 27 wherein:
2 the number of screw flights is a variable selected from the group consisting of
3 two, three, four, five, and six.
- 1 29. A screw extruder comprising :
2 a barrel, said barrel having a bore defining an inner surface; and

3 at least one extruder screw, positioned within said bore, said at least one
4 extruder screw including a central shaft and a plurality of dispersive elements, said
5 dispersive elements being configured and positioned on said at least one extruder
6 screw to form a plurality of progressively narrowing passages through which material
7 is forced into a plurality of regions of high elongational and shear stress.

1 30. The screw extruder of claim 29 wherein:
2 said dispersive elements are positioned in a helical configuration.

1 31. The screw extruder of claim 29 wherein:
2 said screw extruder includes a slip ring and at least one stationary ring.

1 32. The screw extruder of claim 29 wherein:
2 said screw extruder includes a non-return valve.

1 33. The screw extruder of claim 31 wherein:
2 said slip ring includes a plurality of dispersive elements.

1 34. The screw extruder of claim 31 wherein:
2 said stationary ring includes a plurality of dispersive elements

1 35. A method of extruding material from a screw extruder comprising the steps of:
2 providing a screw extruder including a barrel having input and output ends, a
3 bore defining an inner surface, and an extrusion die at said output end;
4 providing at least one extruder screw positioned within said bore, each screw
5 including a central shaft, said at least one extruder screw further including a plurality
6 of dispersive mixing elements which interact with said inner surface of said barrel to
7 form progressively narrowing passages through which material is forced into multiple
8 regions of high elongational and shear stress;
9 introducing extrusion material into said input end of said barrel;
10 rotating said at least one screw to force said material through said dispersive
11 mixing elements where said material passes through multiple regions of high
12 elongational and shear stress; and

13 conveying said material towards said extrusion die at said output end to be
14 shaped.

1 36. The method for extruding material from a screw extruder of claim 35 wherein:
2 said dispersive mixing elements are selected from a group consisting of
3 tapered slots formed in said flights, fluted sections with ramped barrier flights formed
4 on the central shaft, fluted sections with barrier flights formed on said central shaft
5 which are triangular wedge shapes, barrier flights with triangular profile, diamond
6 shaped protrusions, triangular pins, and protrusions which are positioned on a
7 stationary ring and protrusions which are positioned on the interior of a slide ring.

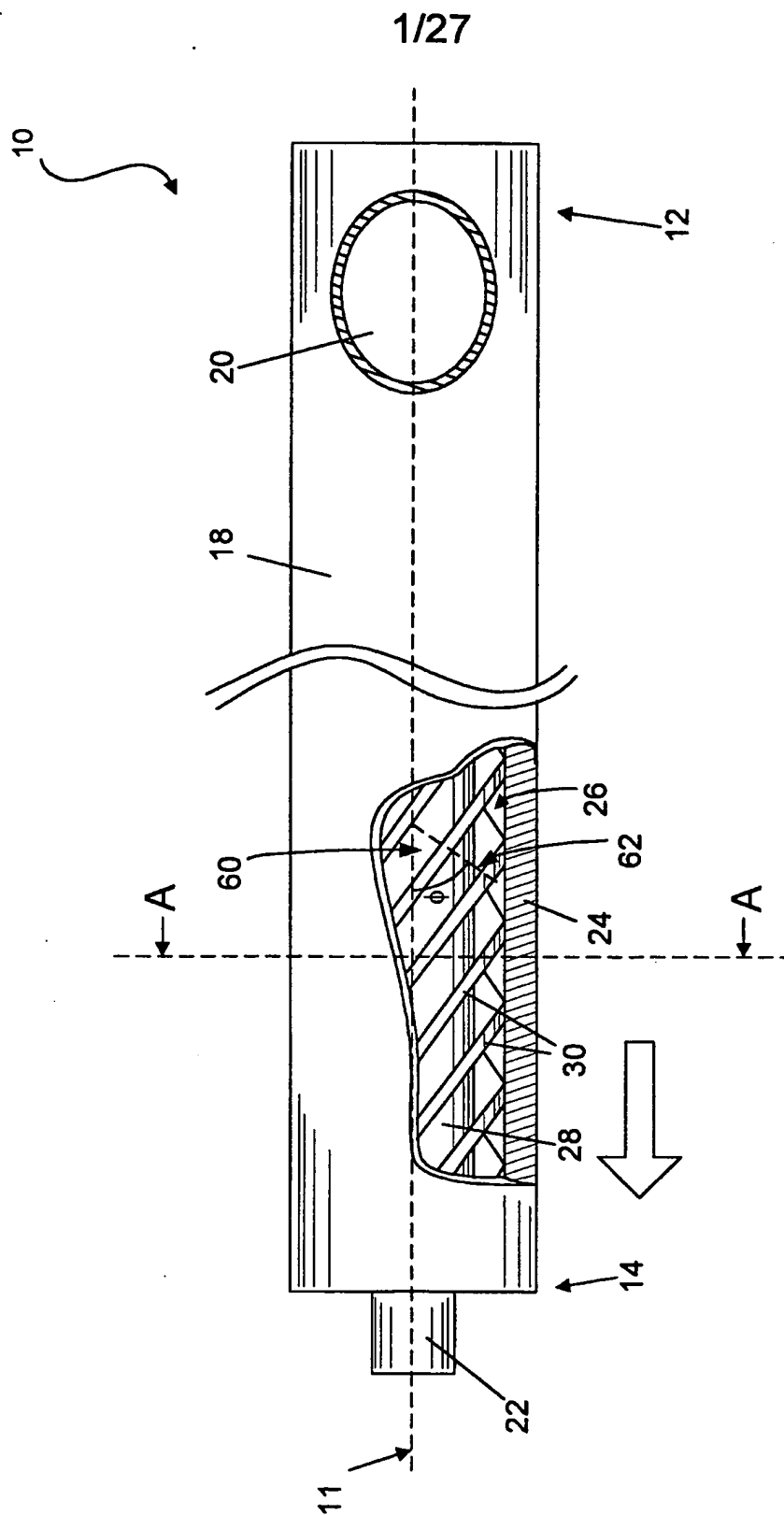


FIGURE 1

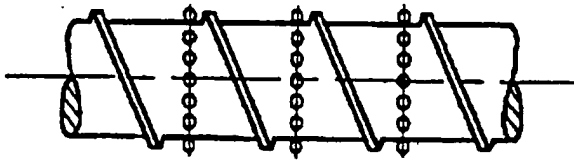


FIG. 2A

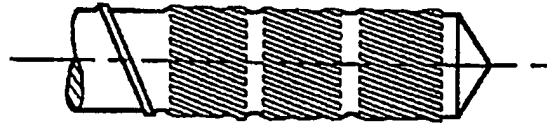


FIG. 2B



FIG. 2C

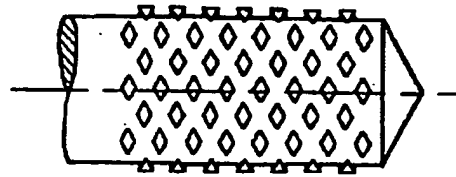


FIG. 2D

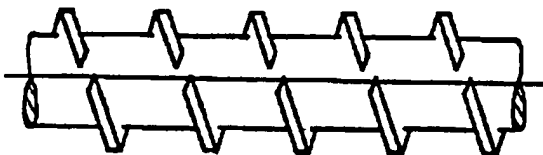


FIG. 2E

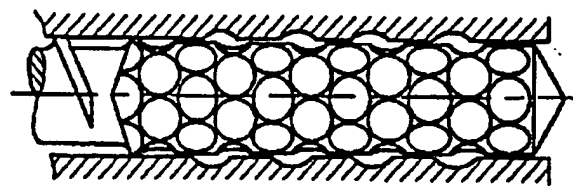


FIG. 2F

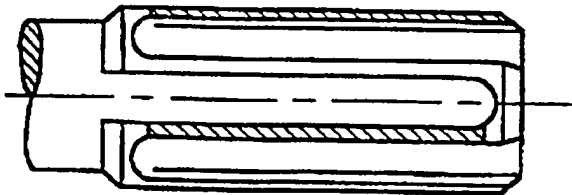


FIG. 2G

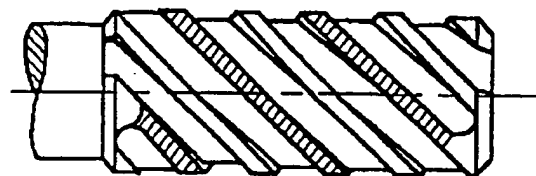


FIG. 2H

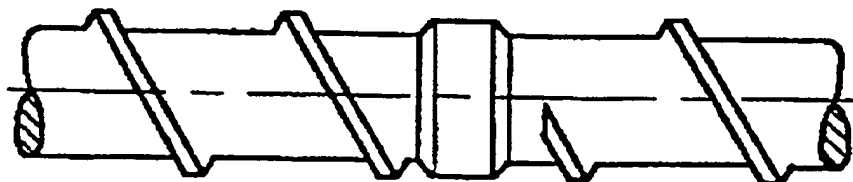


FIG. 2J

FIGURE 2 A-J Prior Art

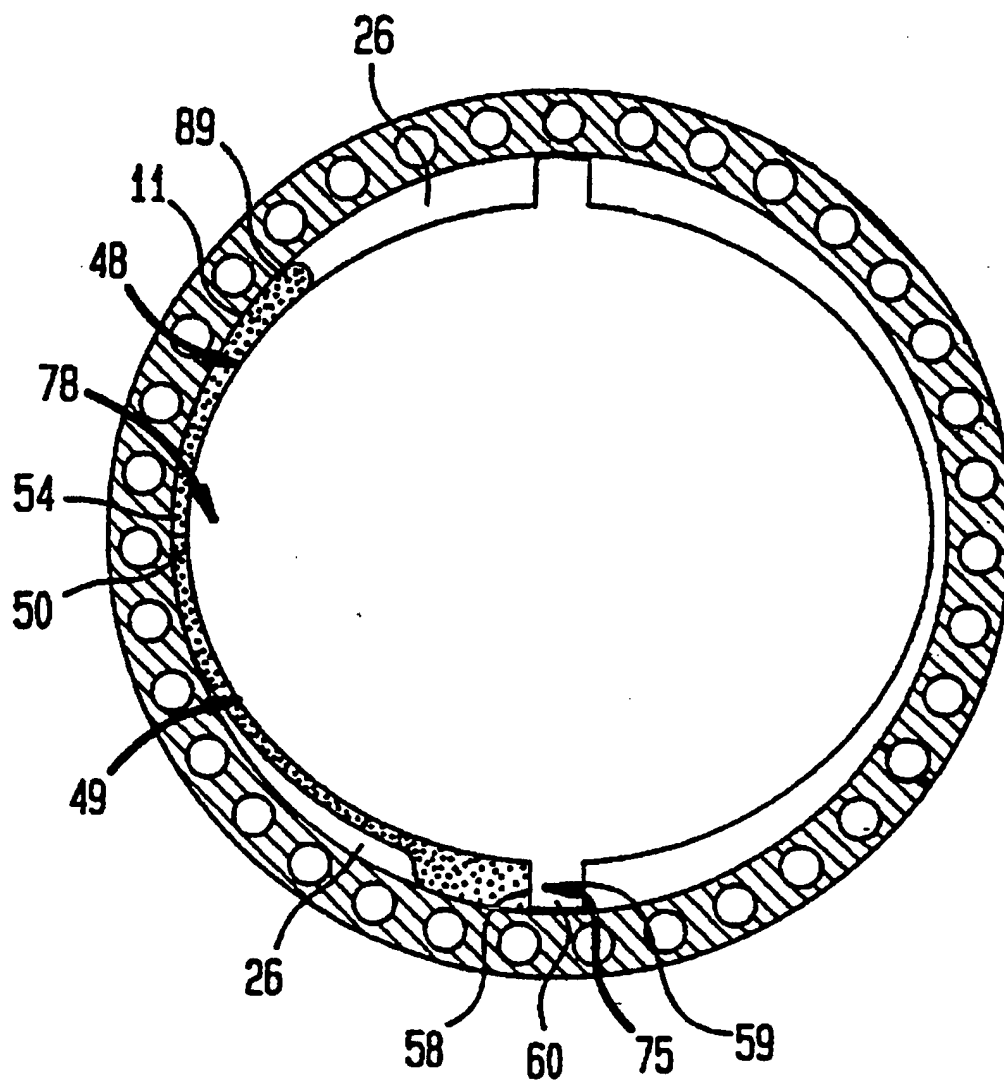


FIGURE 2K Prior Art

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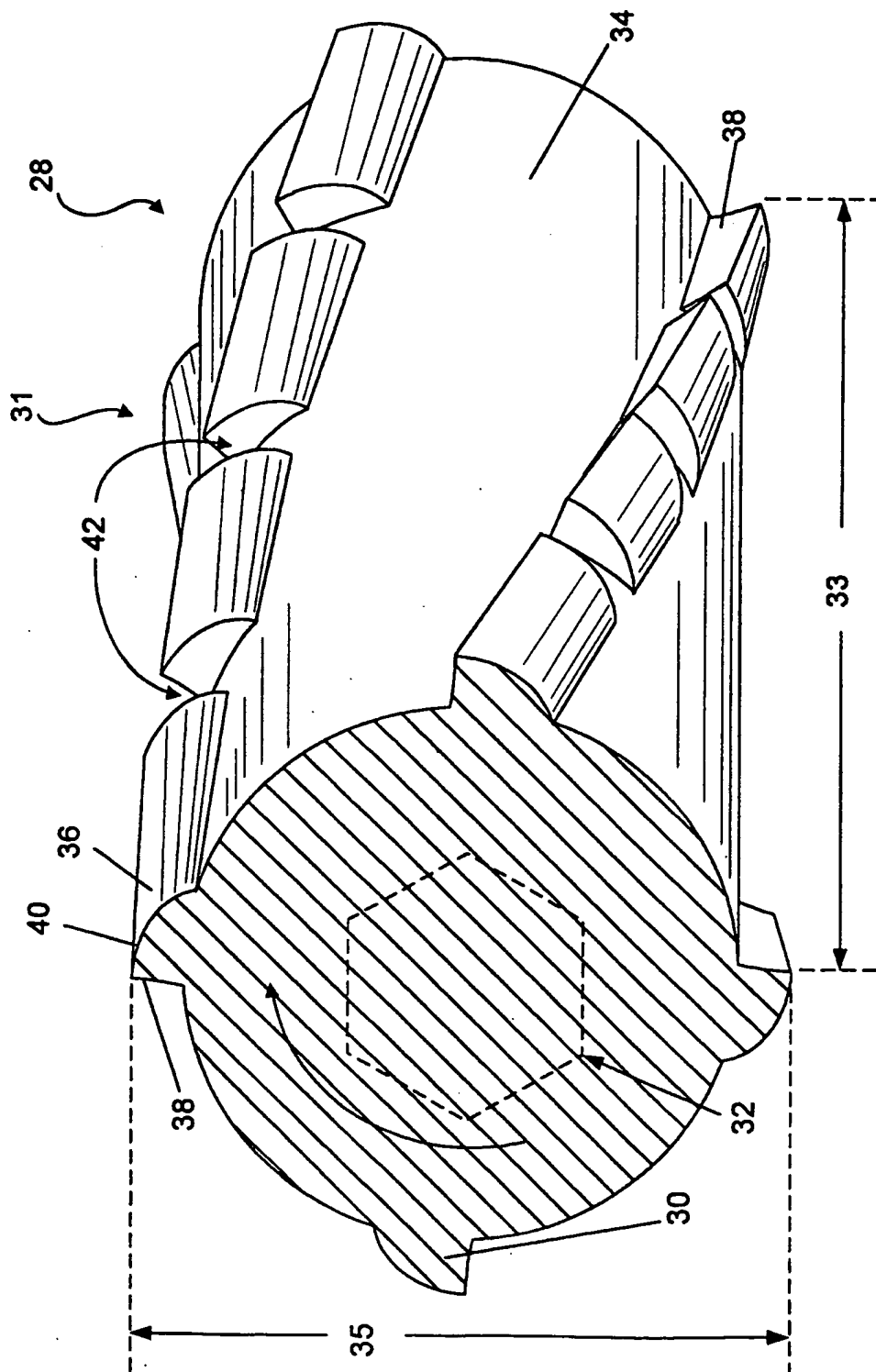


FIGURE 3

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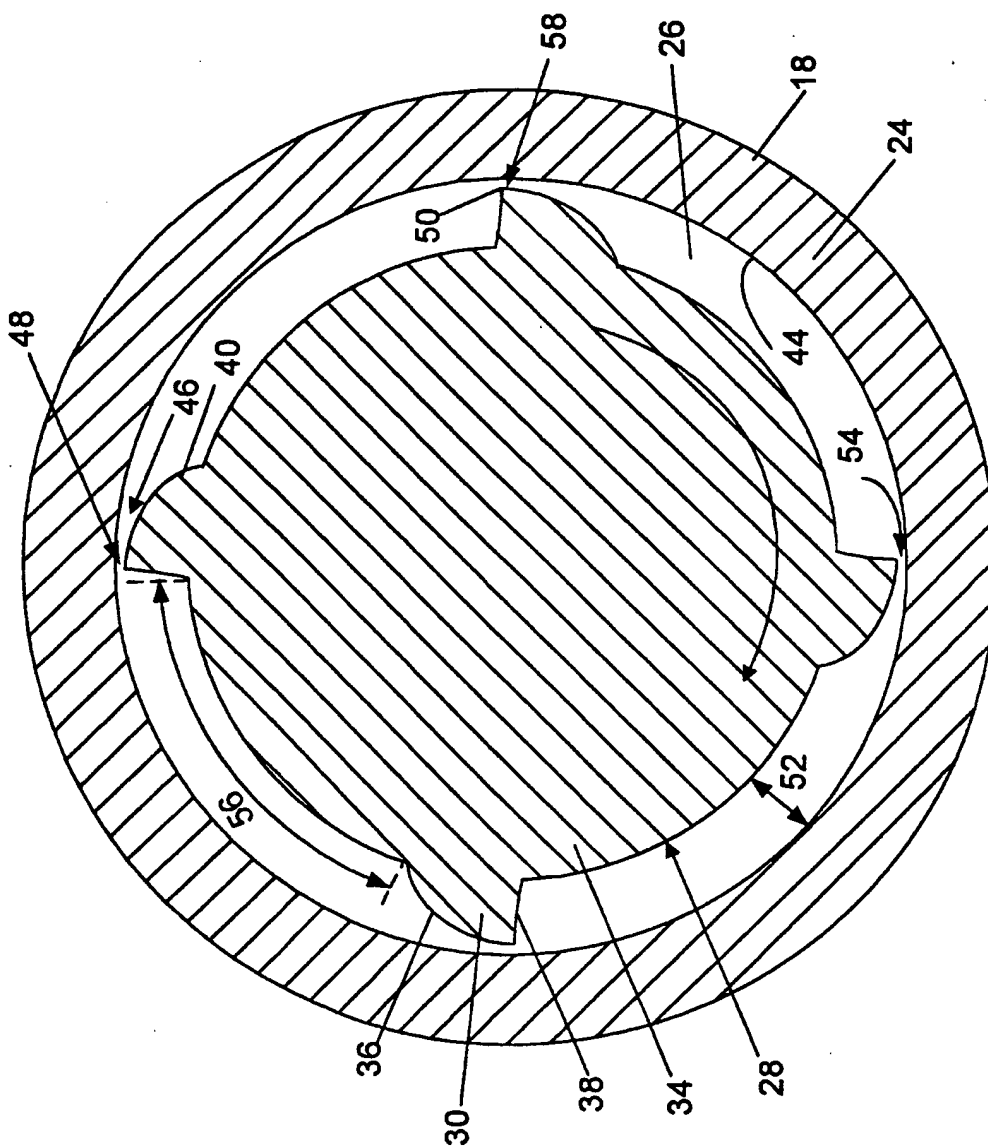


FIGURE 4

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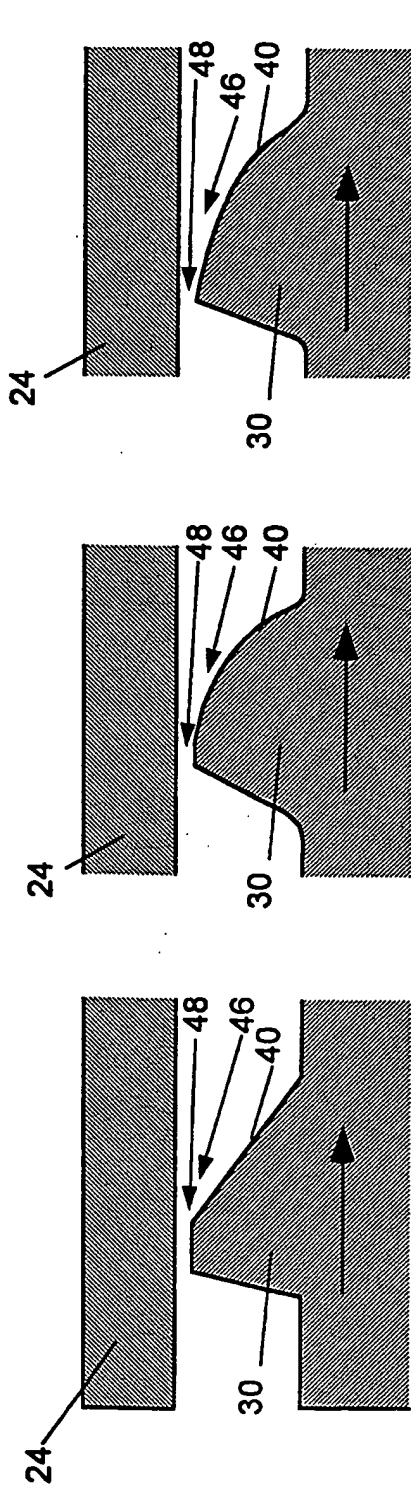


FIG. 5A

FIG. 5B

FIG. 5C

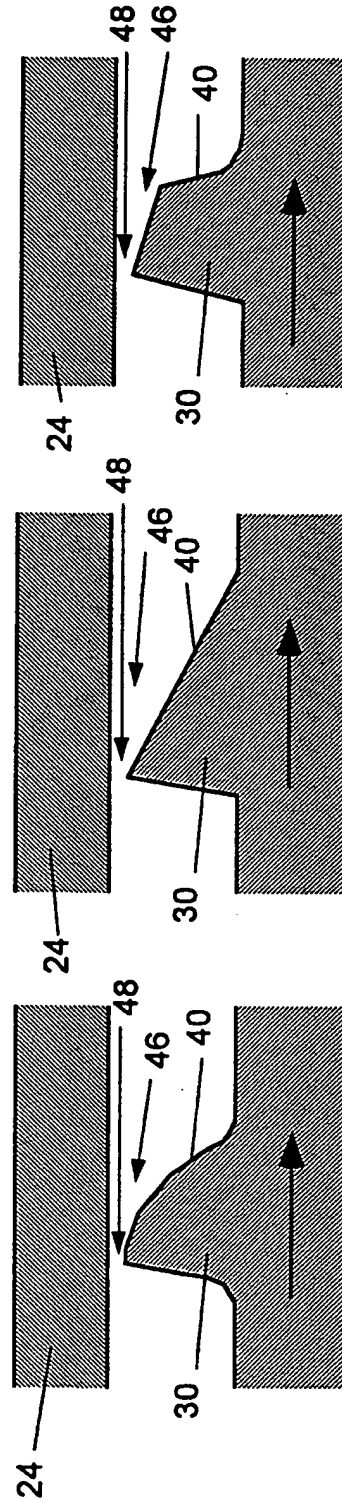


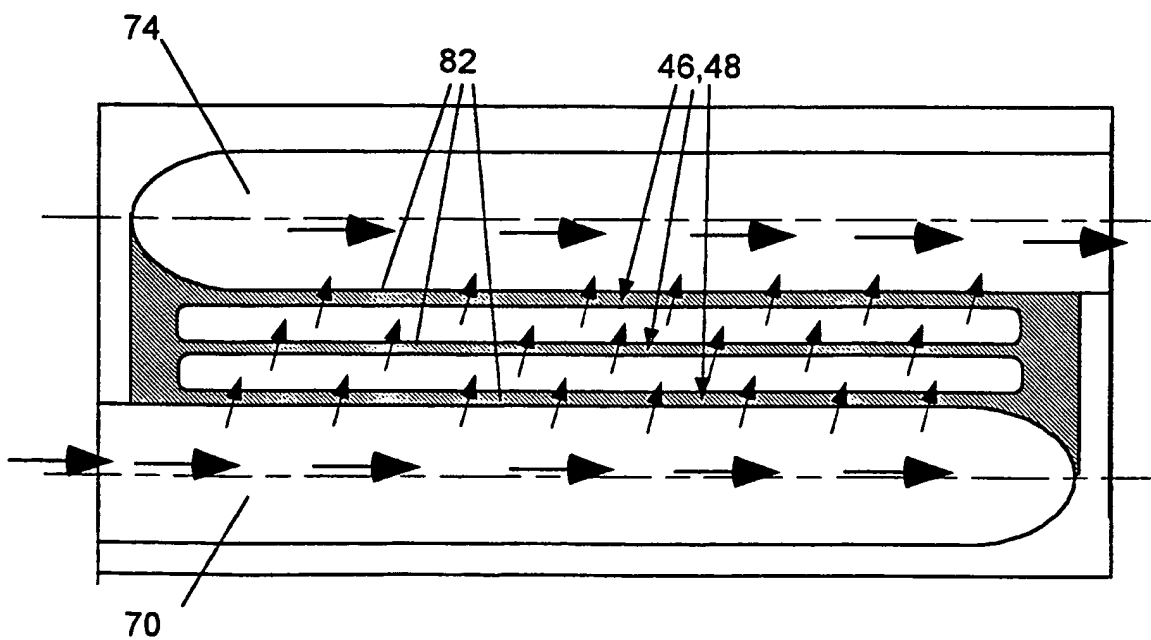
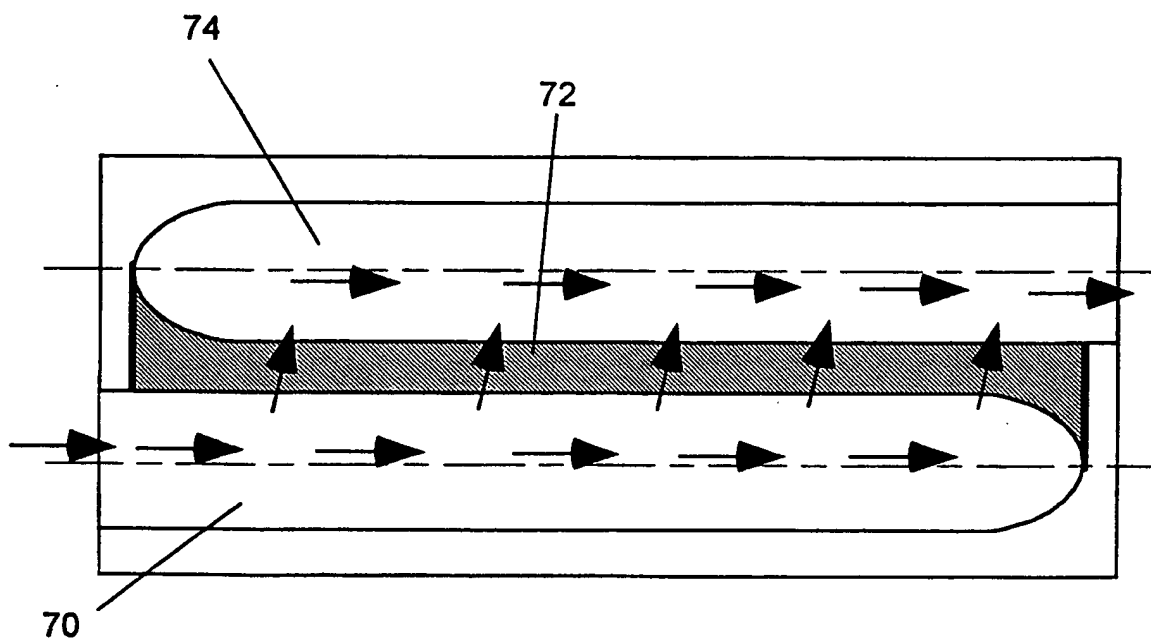
FIG. 5D

FIG. 5E

FIG. 5F

FIGURE 5 A-F

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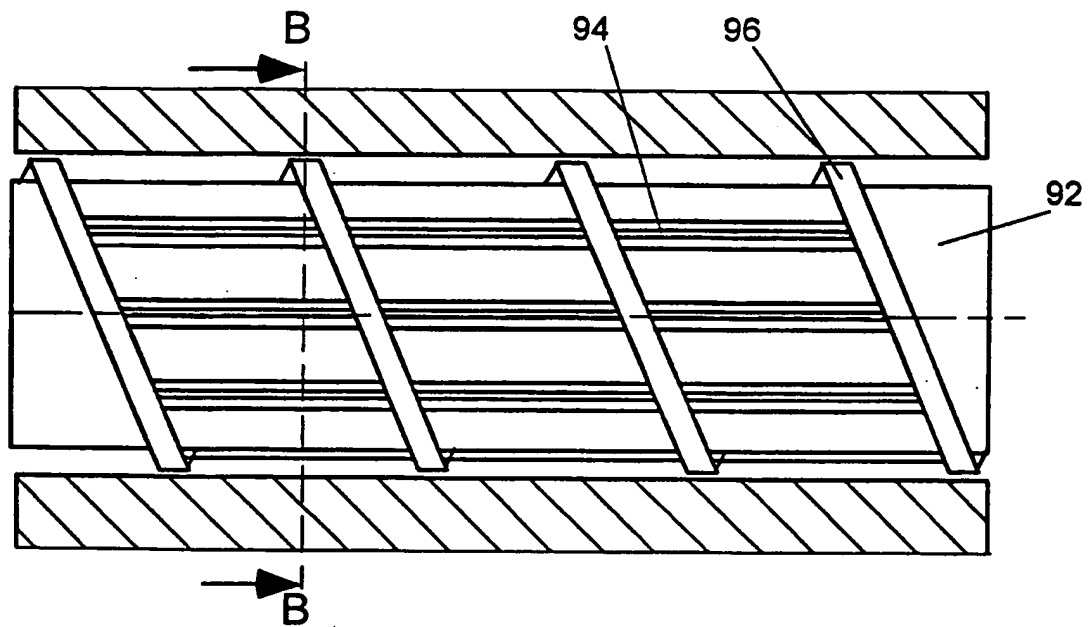


FIGURE 8

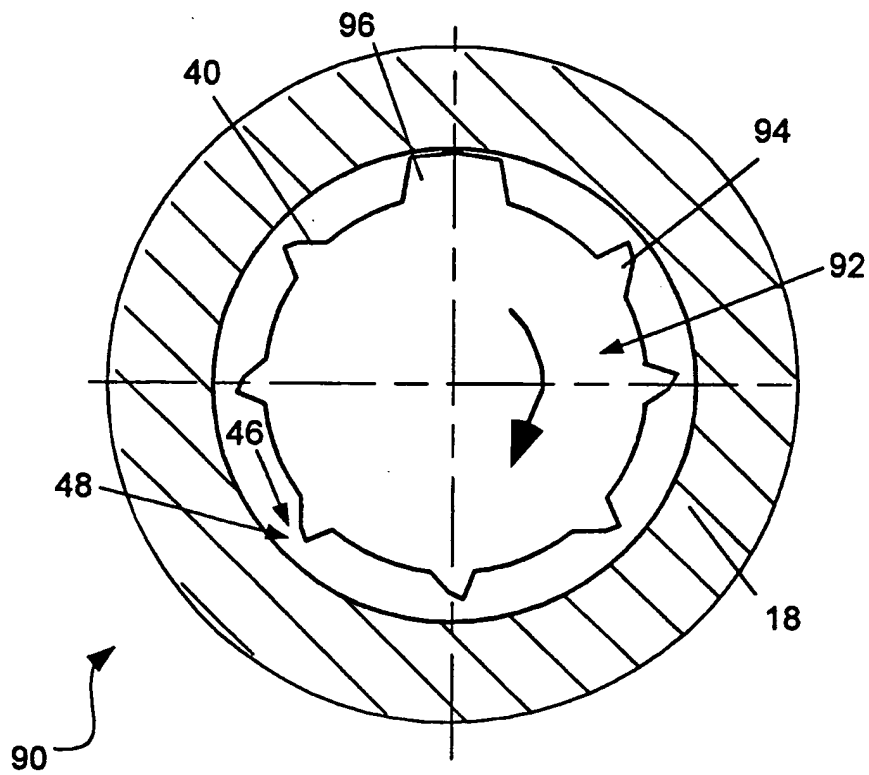


FIGURE 9

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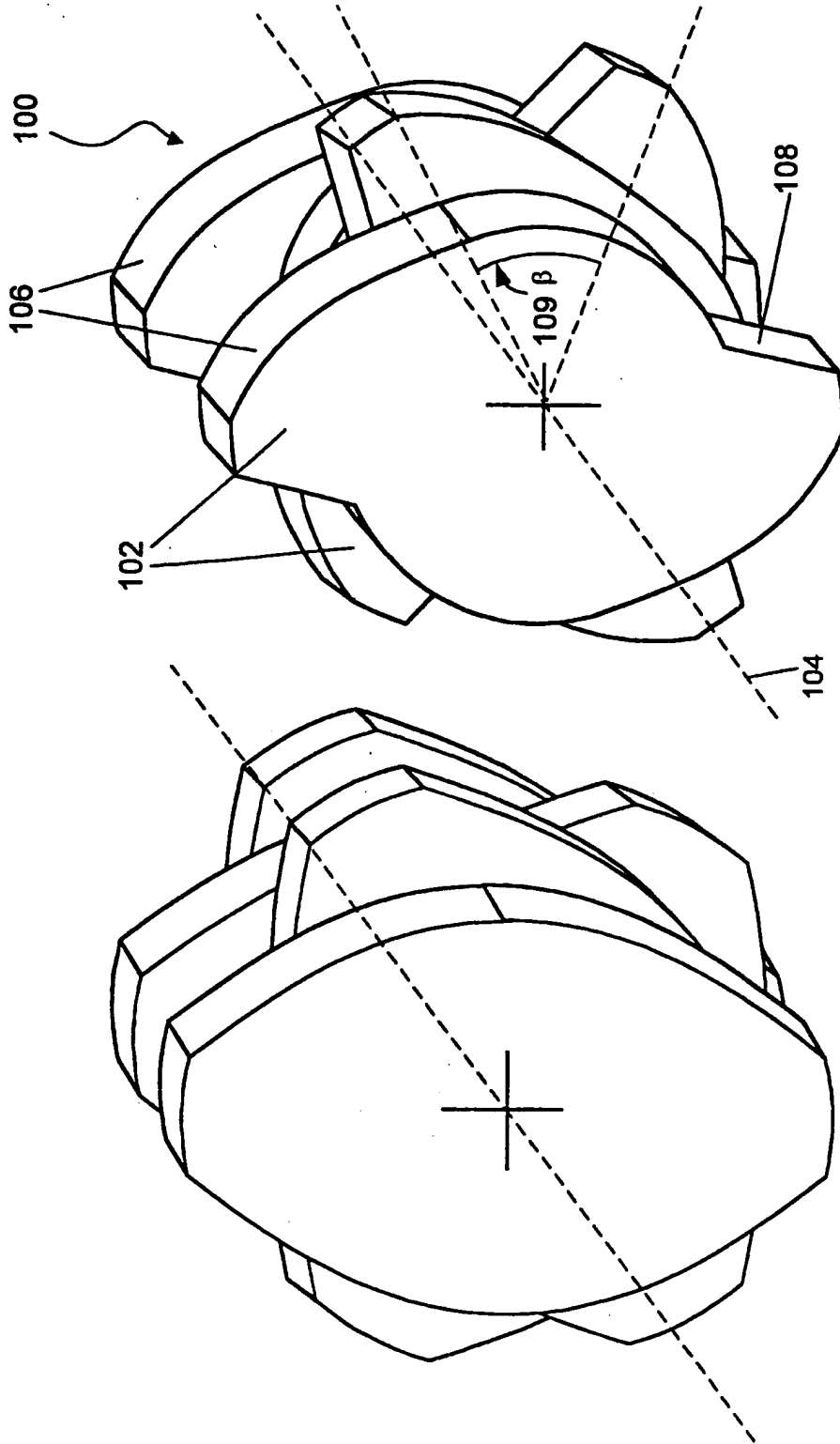


FIGURE 11

FIGURE 10 Prior Art

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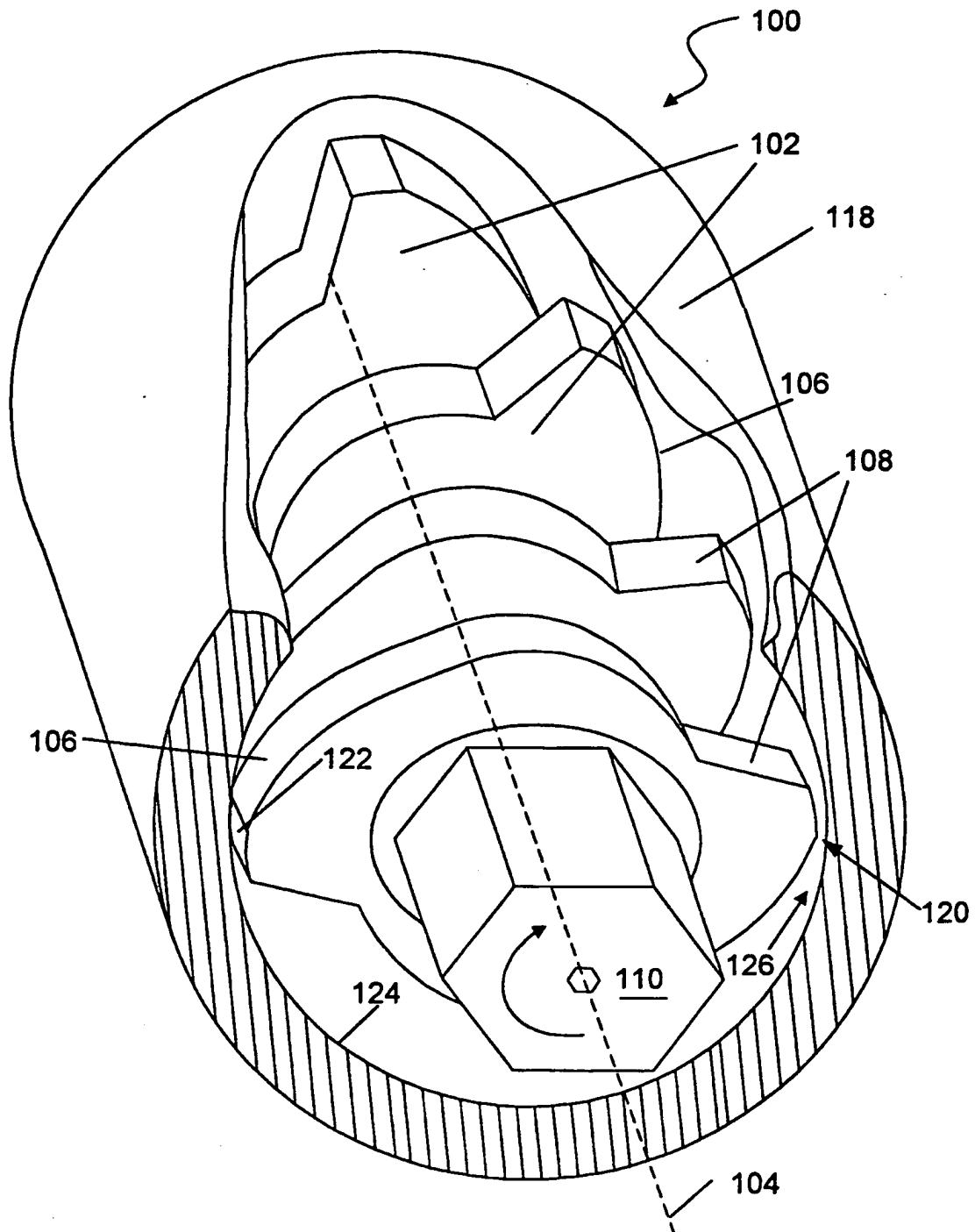


FIGURE 12

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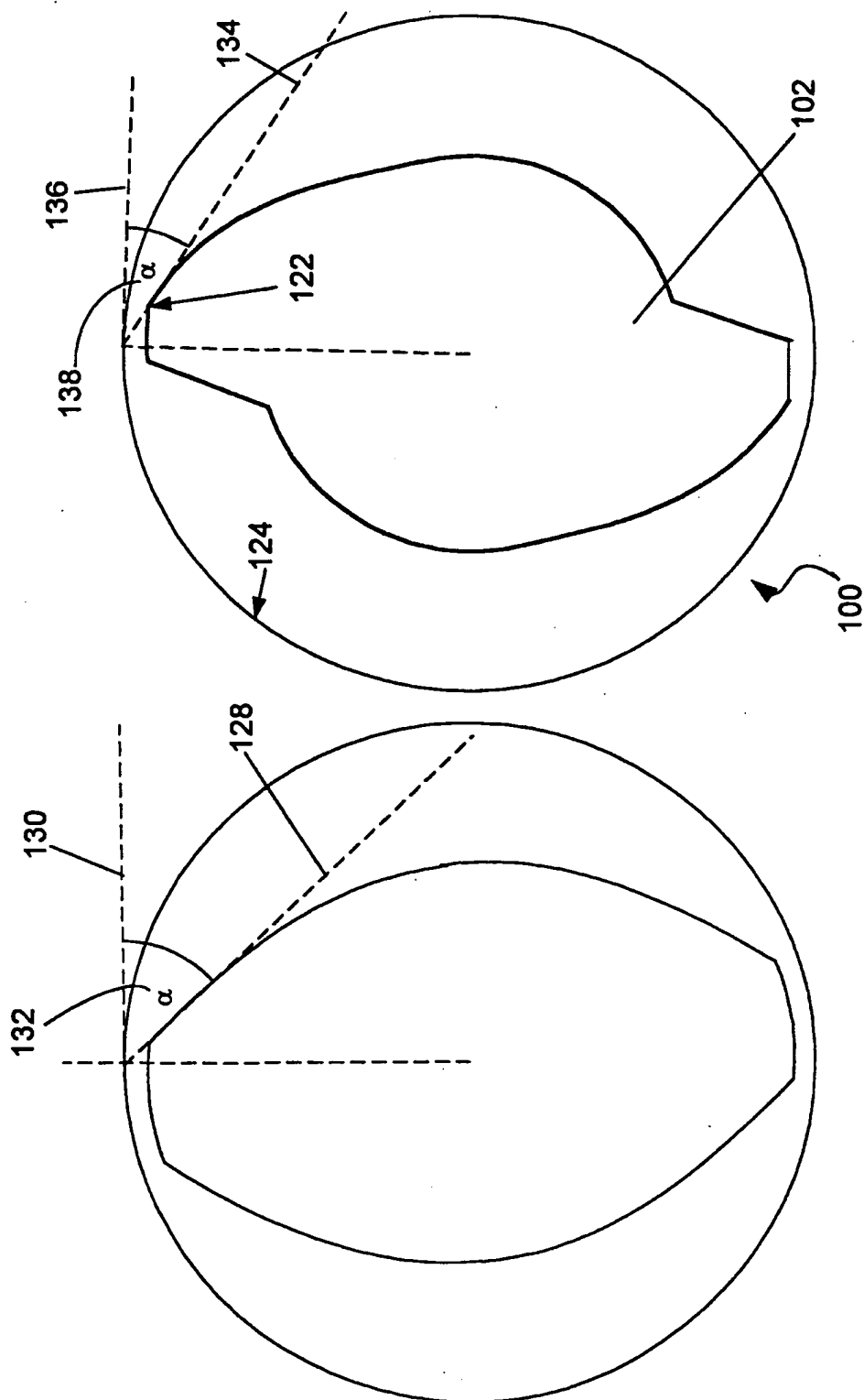


FIGURE 14

FIGURE 13 Prior Art

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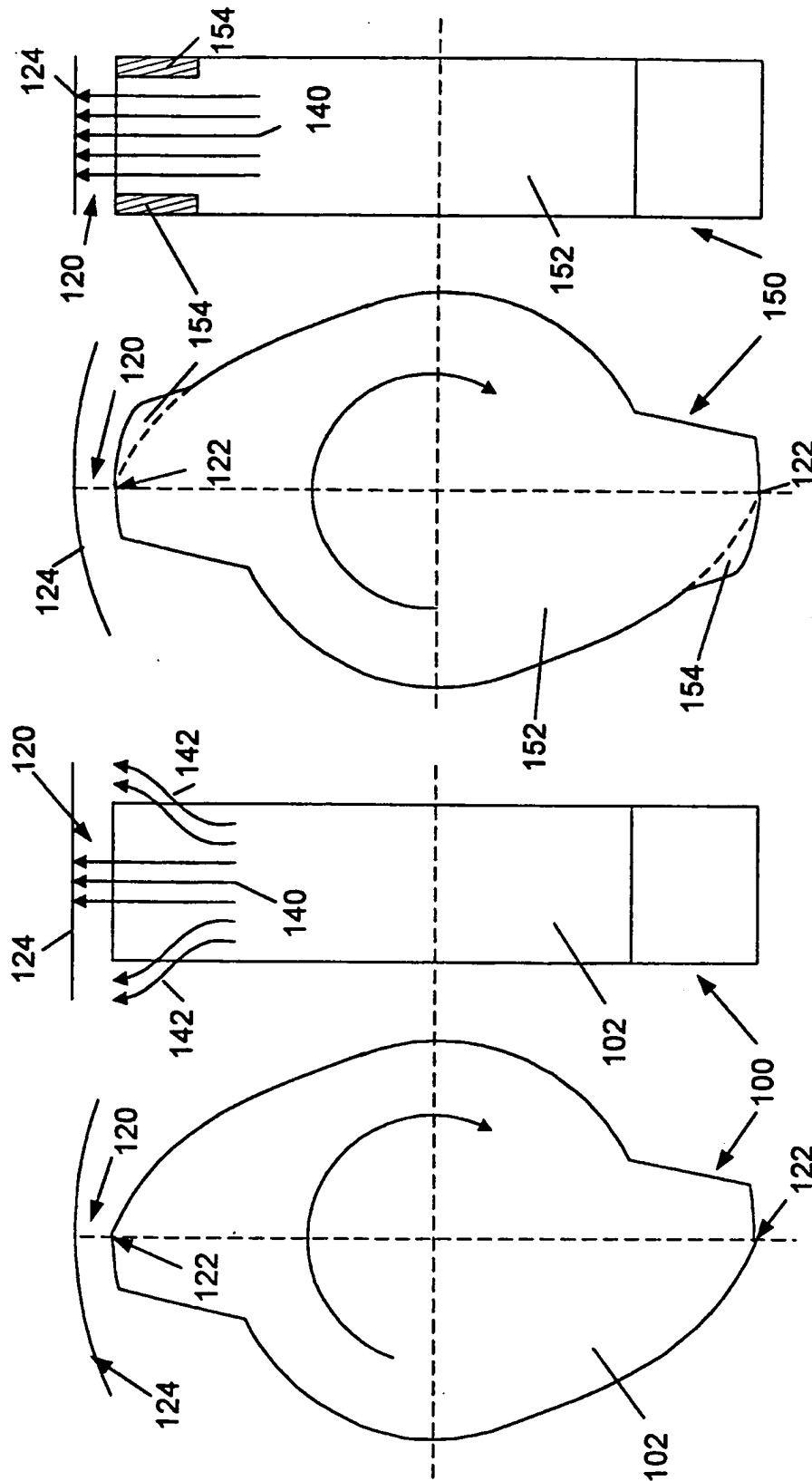


FIGURE 15A FIGURE 15B FIGURE 16B

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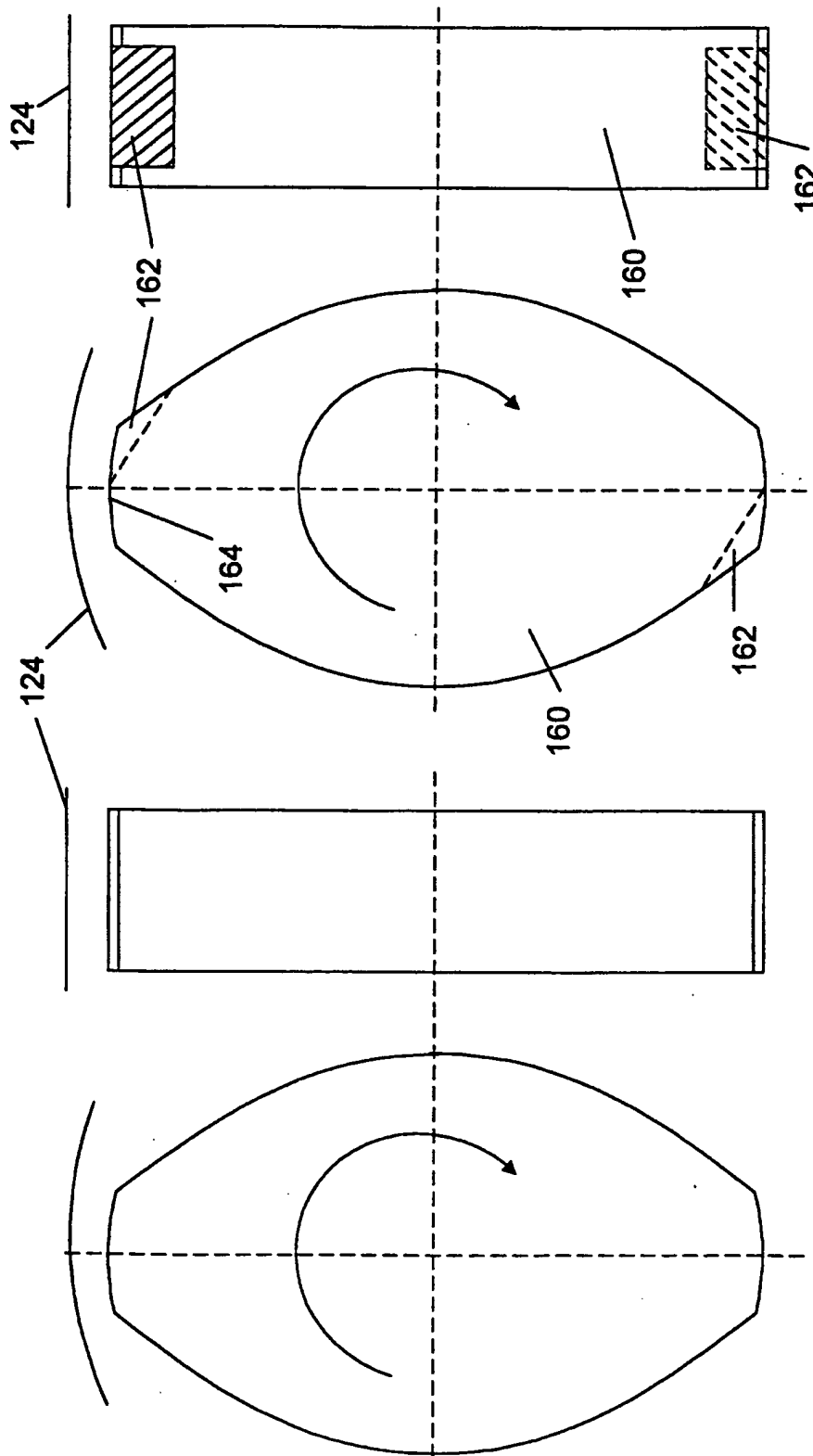


FIGURE 17A Prior Art

FIGURE 18A FIGURE 18B

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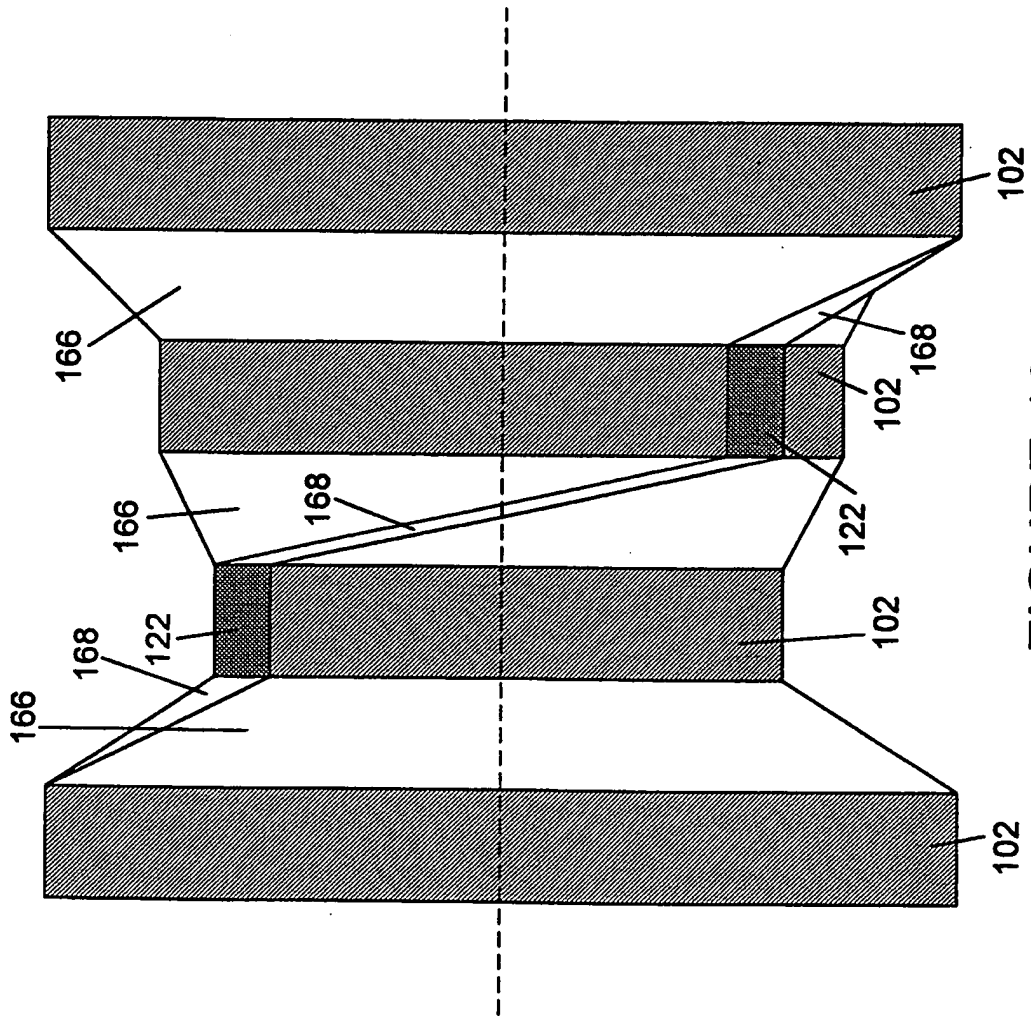


FIGURE 19

FIGURE 20

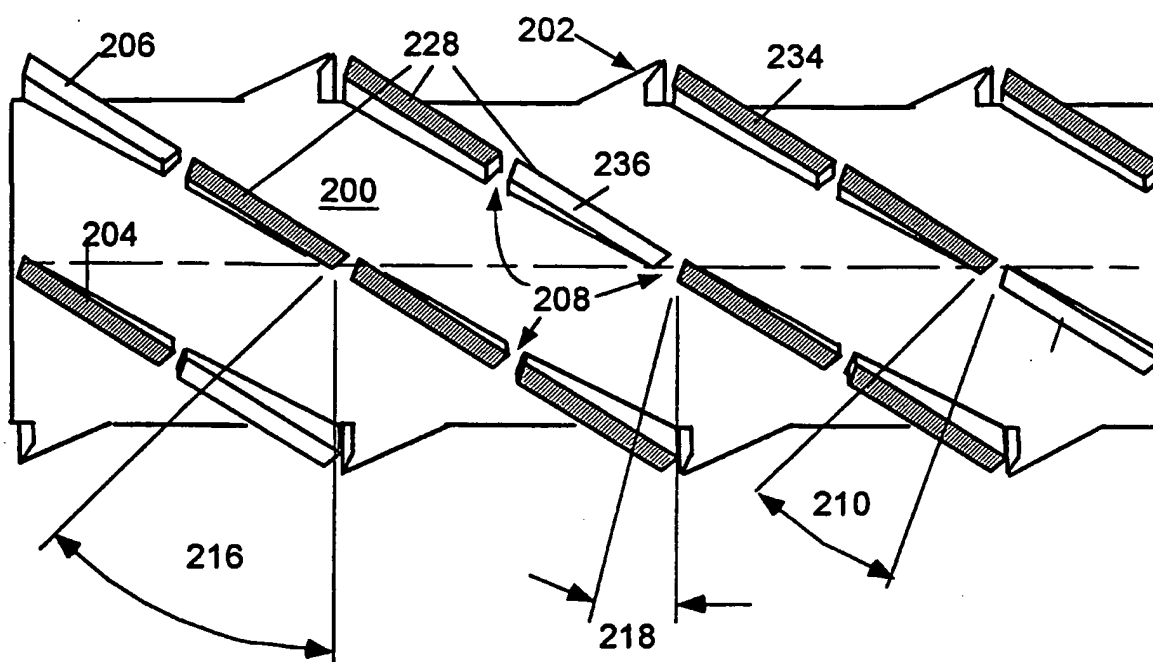


FIGURE 21

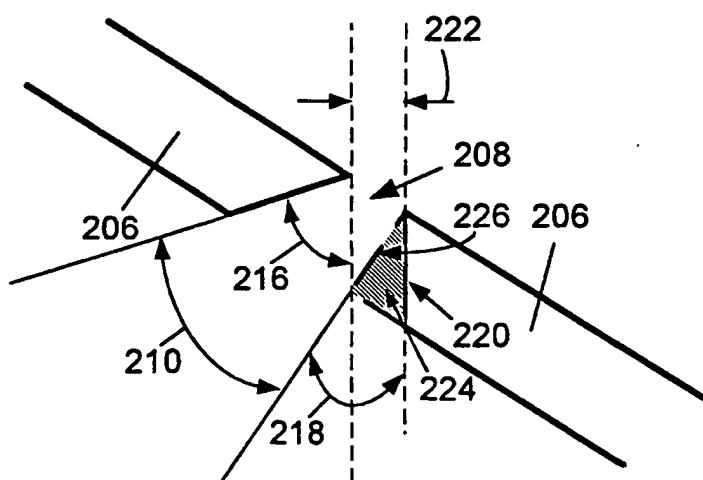


FIGURE 22

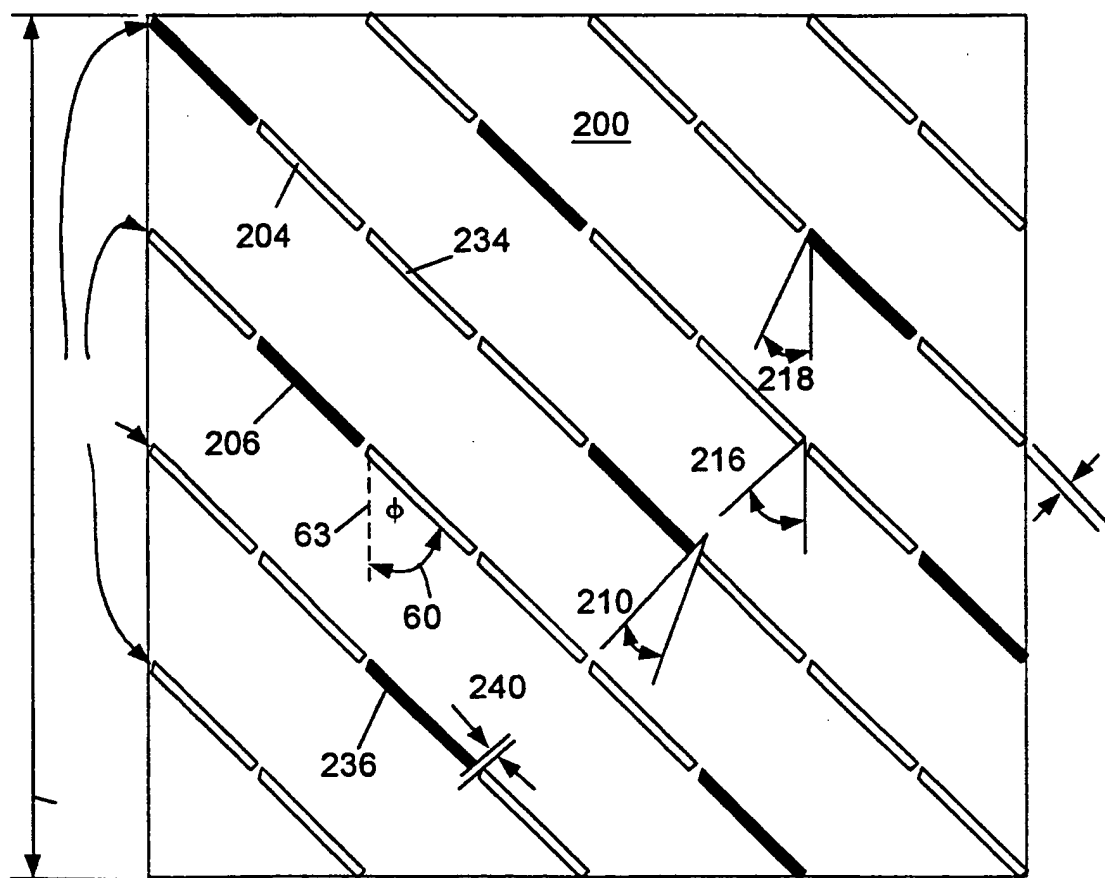


FIGURE 23

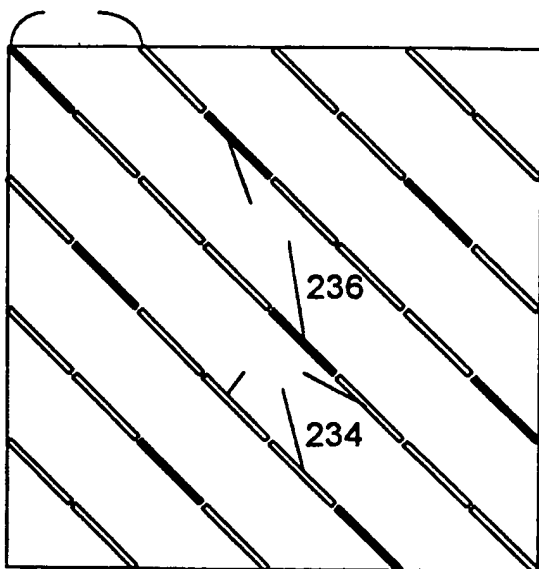


FIGURE 24A

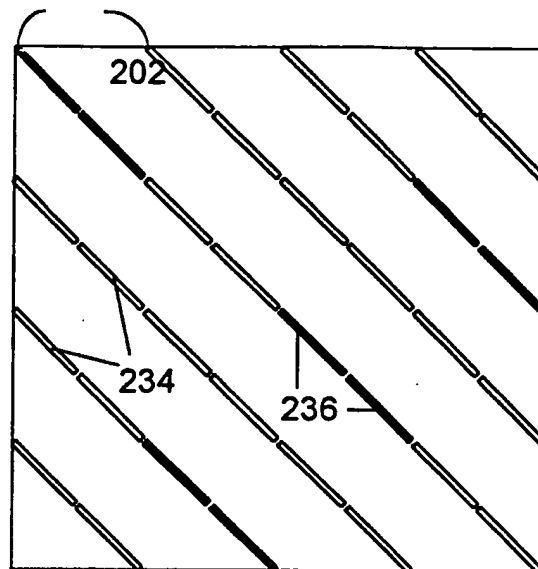


FIGURE 24B

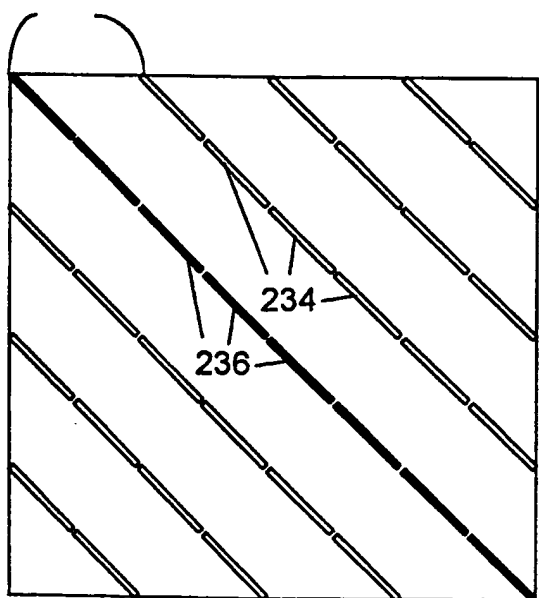


FIGURE 24C

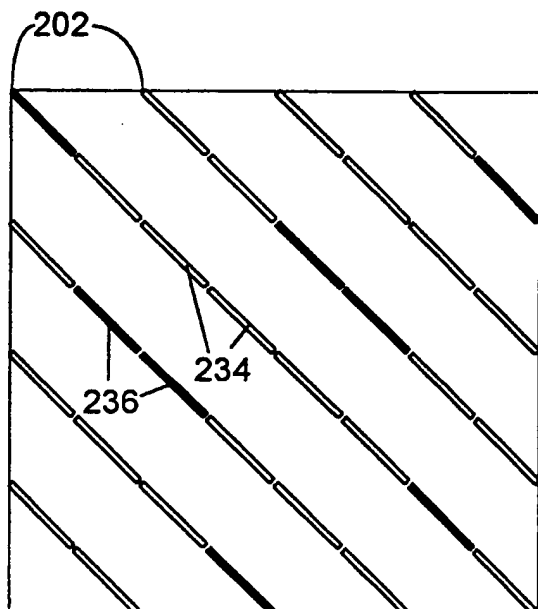


FIGURE 24D

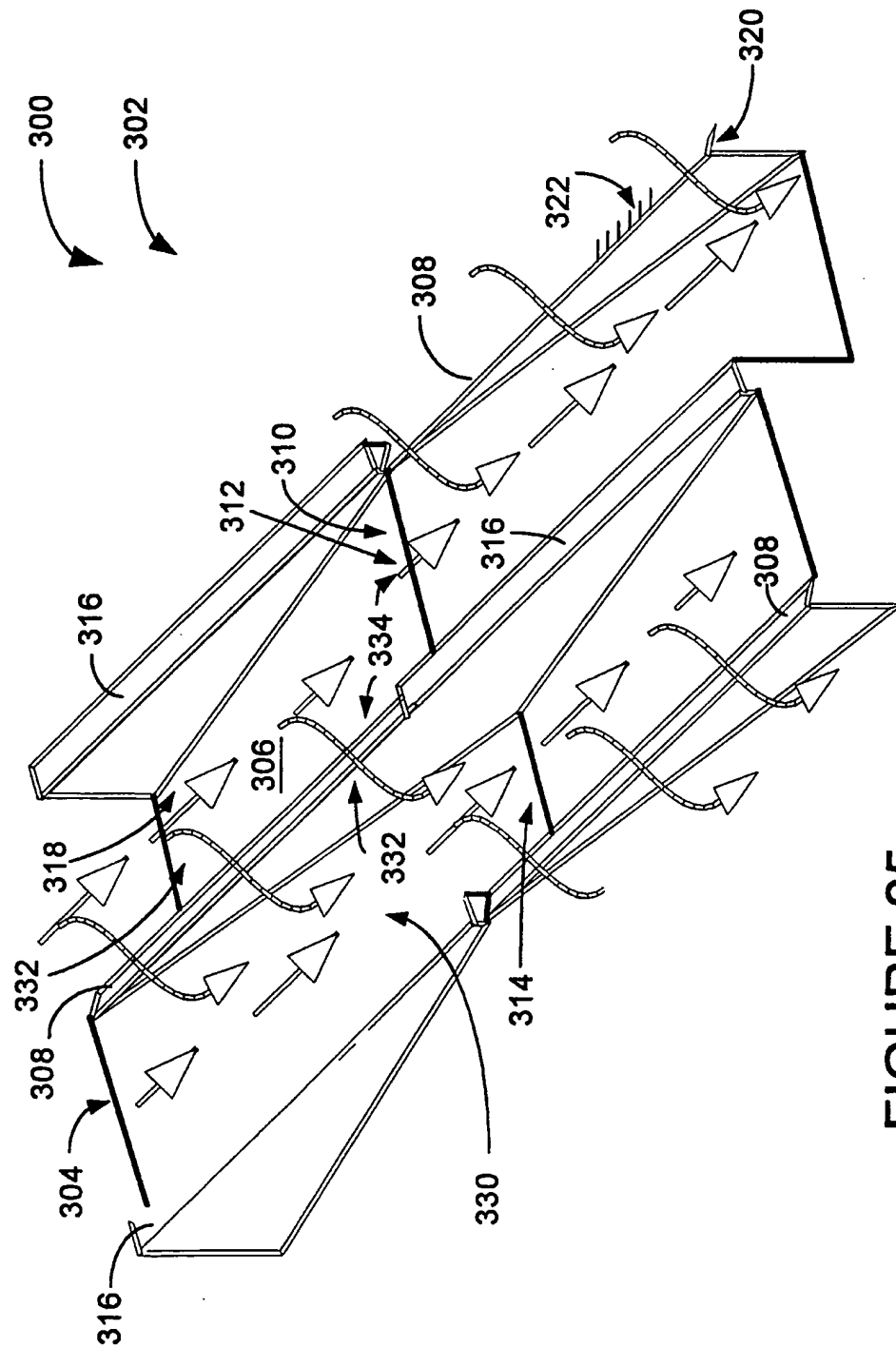


FIGURE 25



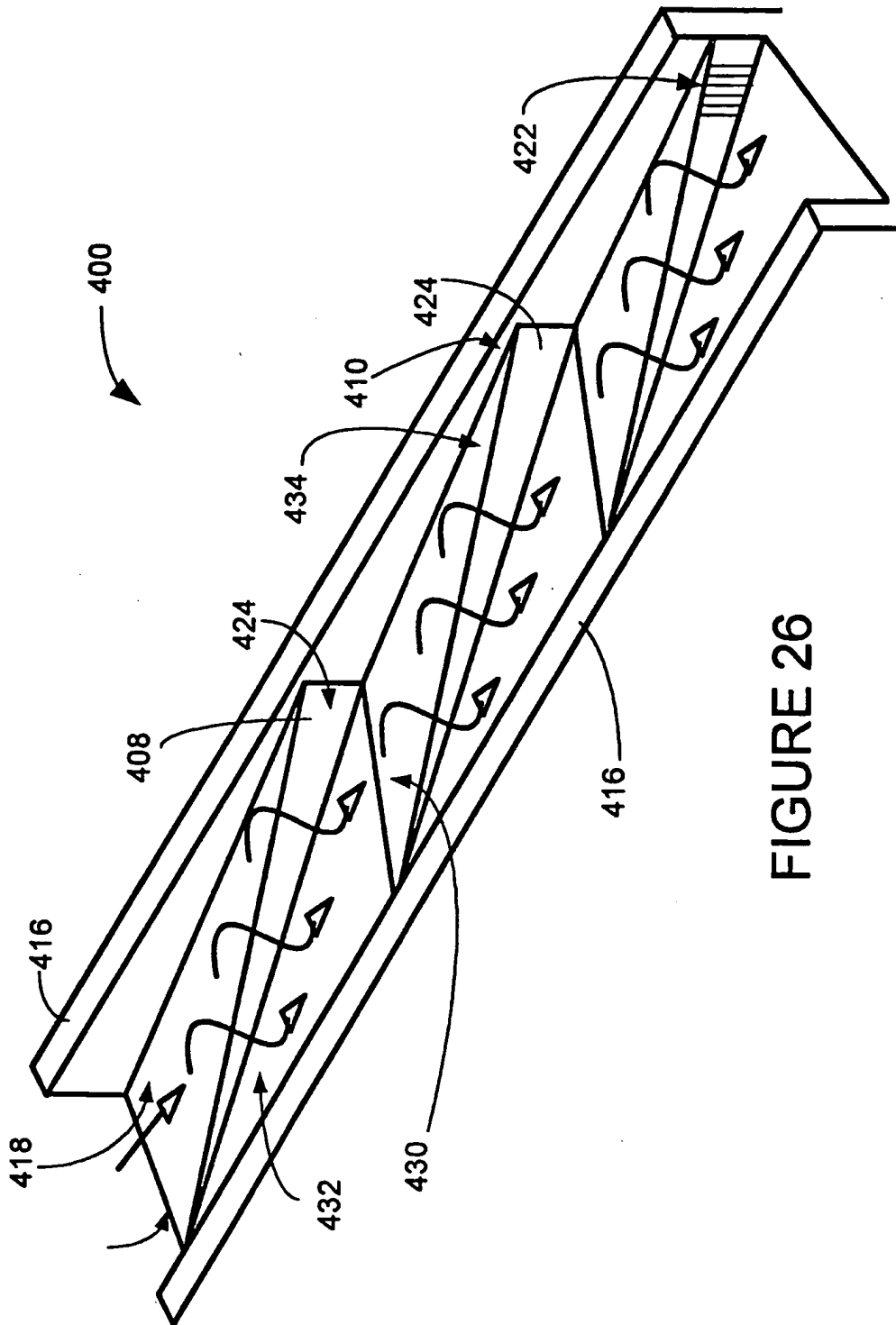


FIGURE 26

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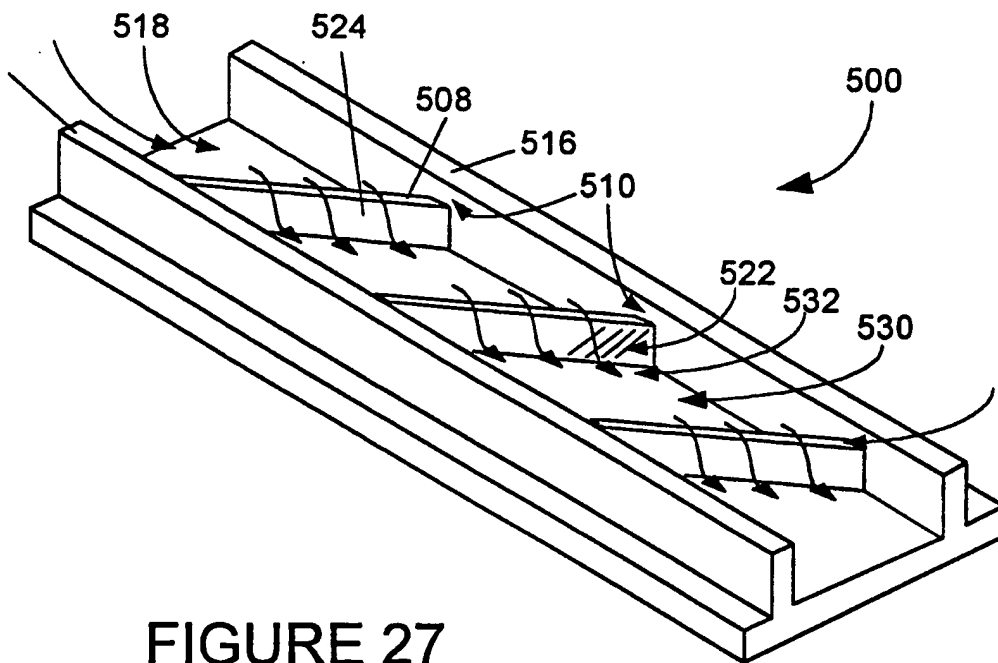


FIGURE 27

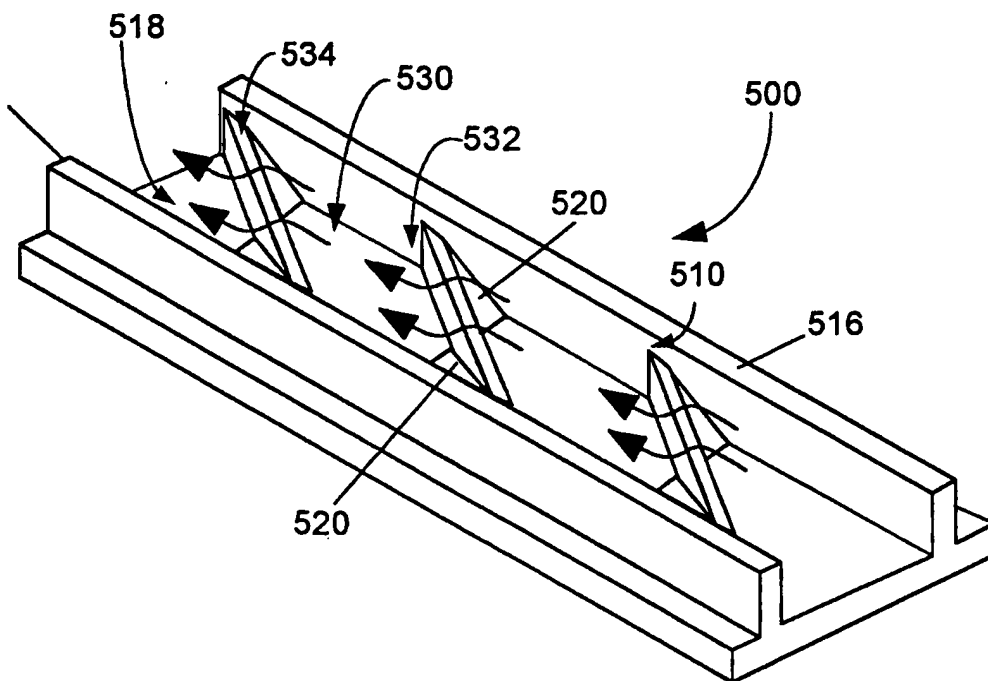


FIGURE 28

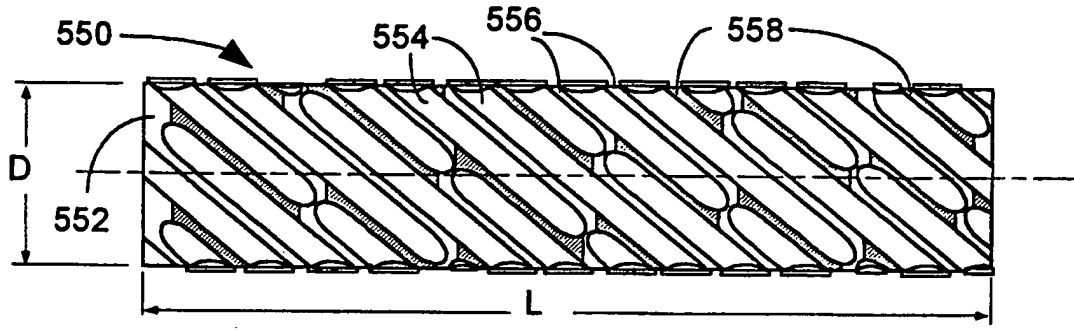


FIGURE 29

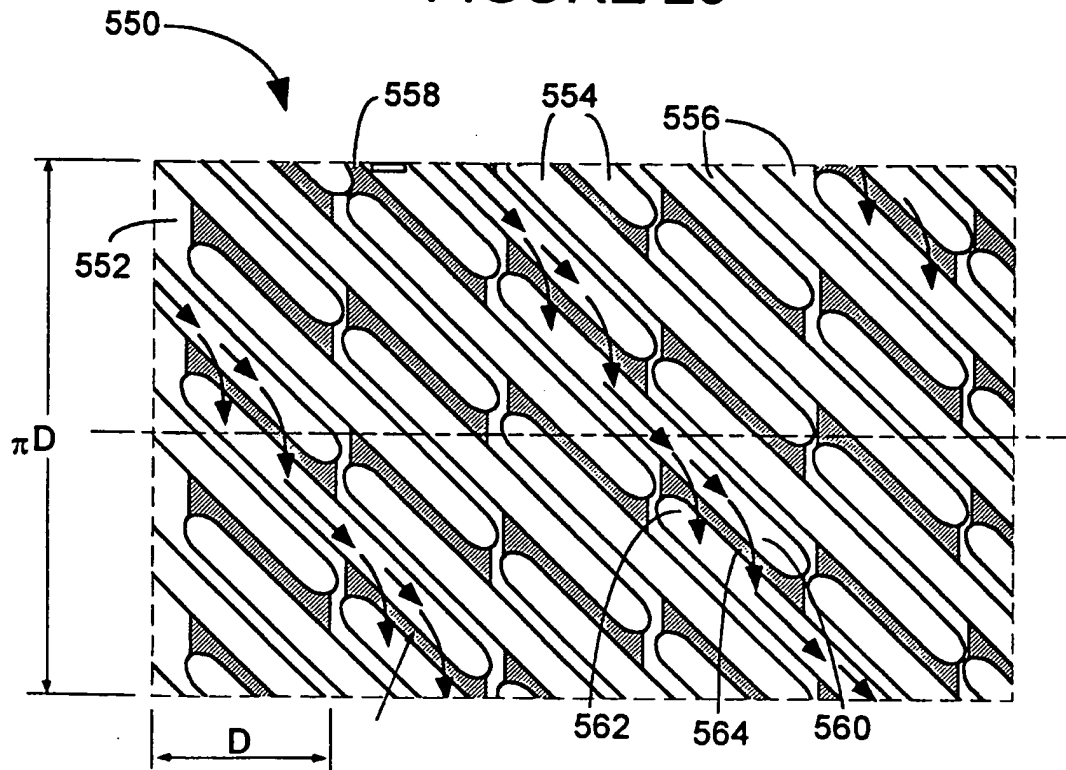


FIGURE 30

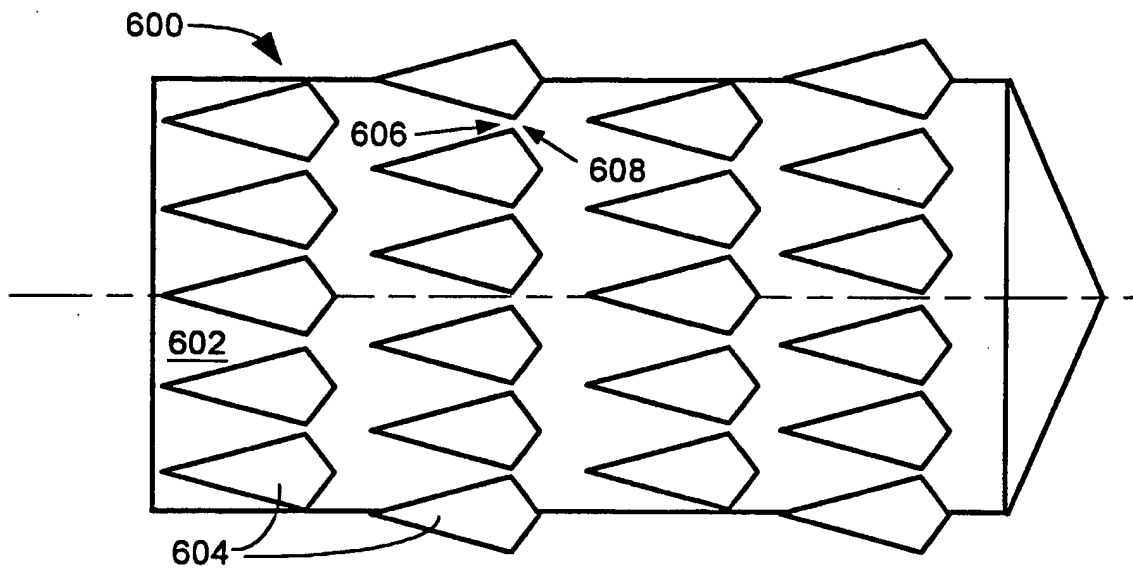


FIGURE 31

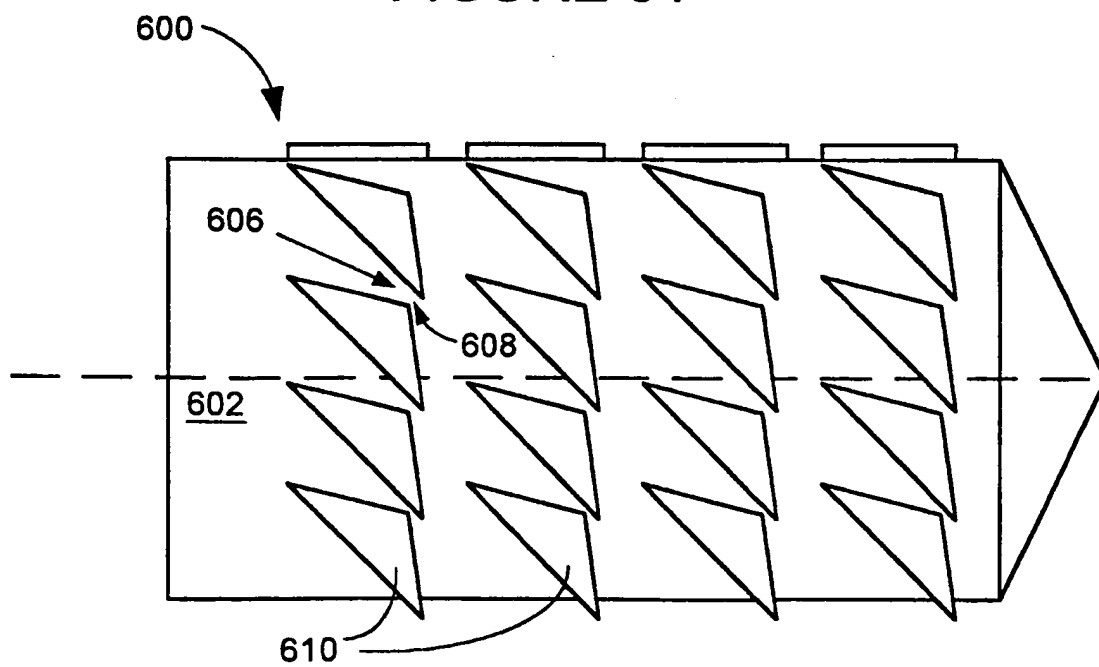


FIGURE 32

FIGURE 33

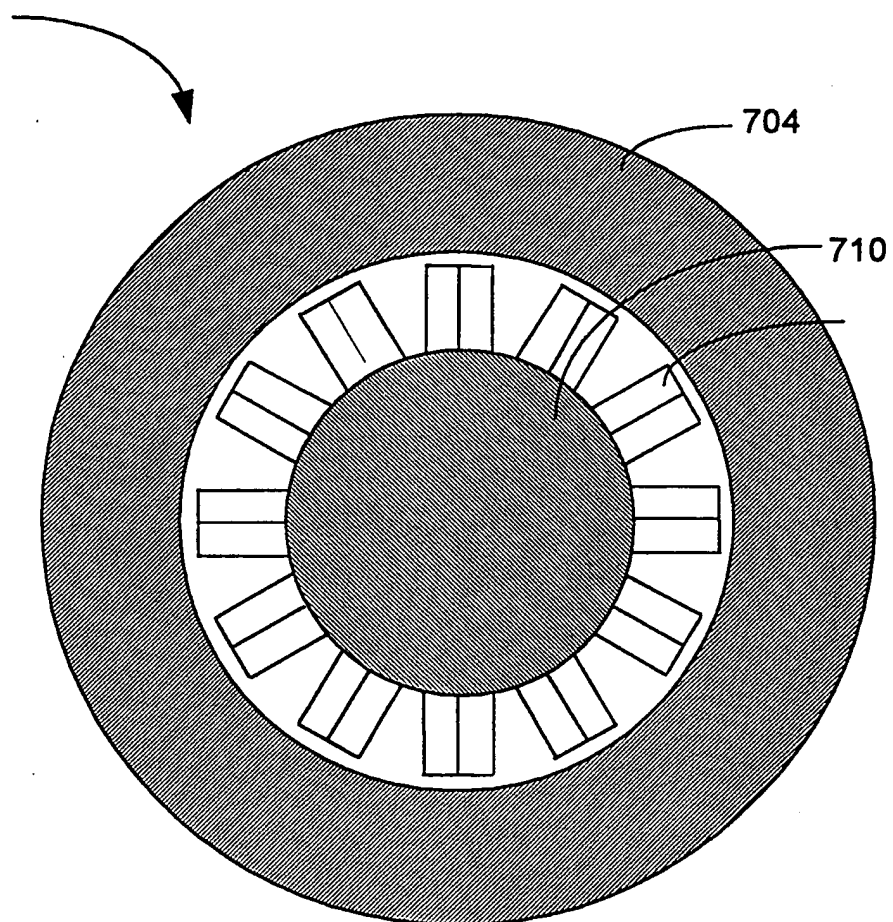


FIGURE 34

FIGURE 35

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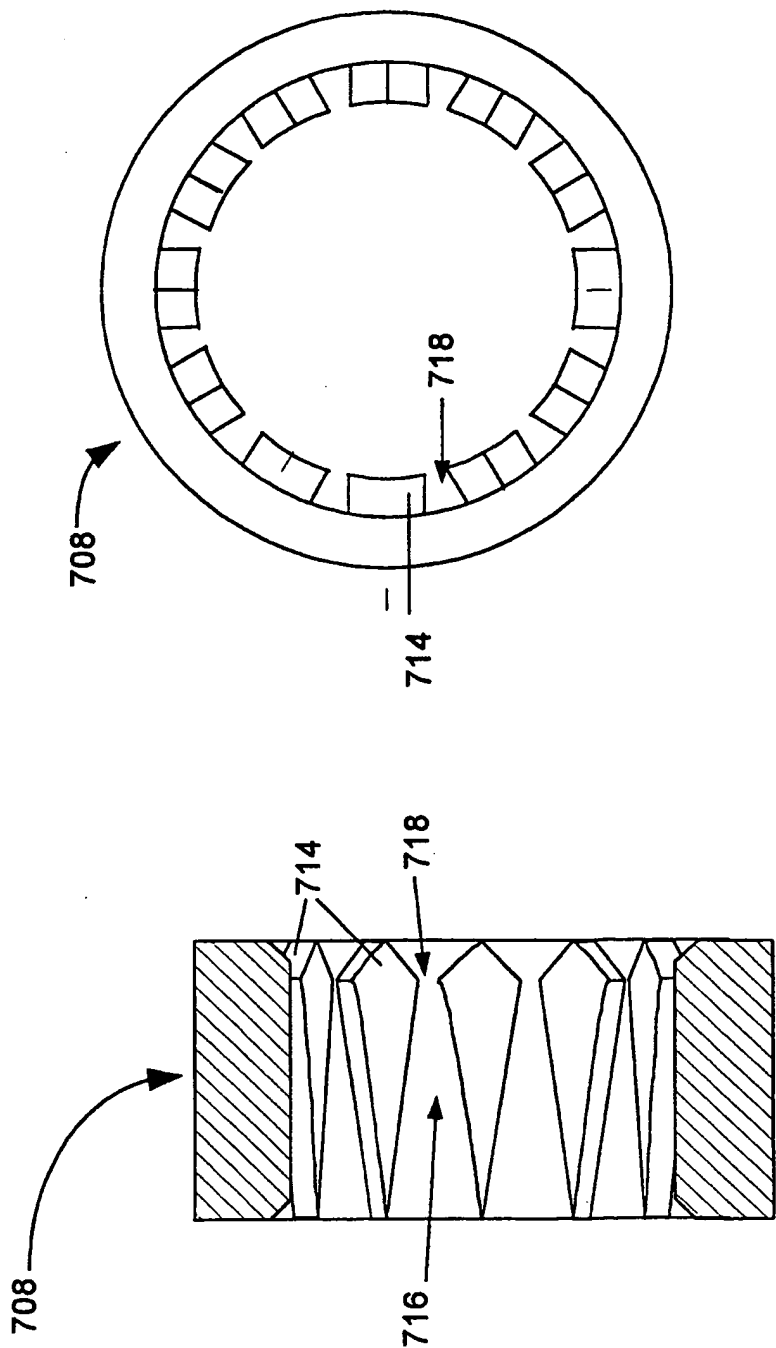


FIGURE 37

FIGURE 36

INTERNATIONAL SEARCH REPORT

International application No.
PCT/US00/02555

A. CLASSIFICATION OF SUBJECT MATTER

IPC(7) : B29C 47/60, 47/62, 47/66

US CL : Please See Extra Sheet.

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 264/211.21, 211.23, 349; 366/79, 81, 84, 85, 89, 300, 301, 318, 319, 322, 323, 324; 425/200, 204, 208, 209

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched
NONE

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)
NONE

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	US 5,356,208 A (TADMOR) 18 October 1994.	1-36

☐ Further documents are listed in the continuation of Box C. ☐ See patent family annex.

* Special categories of cited documents:	*T* later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
A document defining the general state of the art which is not considered to be of particular relevance	*X* document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
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